

# Selective Deposition of Pd onto Silica Supported Iron for Maintaining $\text{Fe}^0$ during Hydrodeoxygenation

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**SECS**

**September 23, 2019**

# Outline

- Motive and Background
- Target and Challenges
- Potential Solution: Pd-Fe
- Strong Electrostatic Adsorption (SEA)
- SEA on silica-supported  $\text{Fe}_2\text{O}_3$
- Synthesis and Characterization
  - Uptake Surveys
  - Temperature Programmed Reduction
  - In-Situ XRD reduction
- Conclusions

# Biomass to drop-in fuel: step 1



Cellulose  
Hemicellulose  
Lignin

Pyrolysis

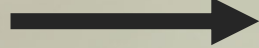


Photo by Dennis Schroeder, NREL 20404. Reliable Characterization for Pyrolysis Bio-Oils Leads to Enhanced Upgrading Methods.

<https://www.nrel.gov/research/highlights/reliable-characterization-pyrolysis.html>.

# Biomass to drop-in fuel: step 2

Remove oxygen from bio-oil

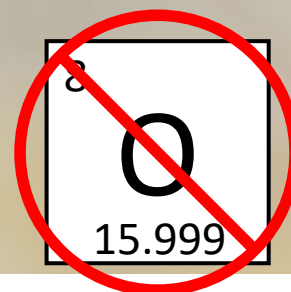
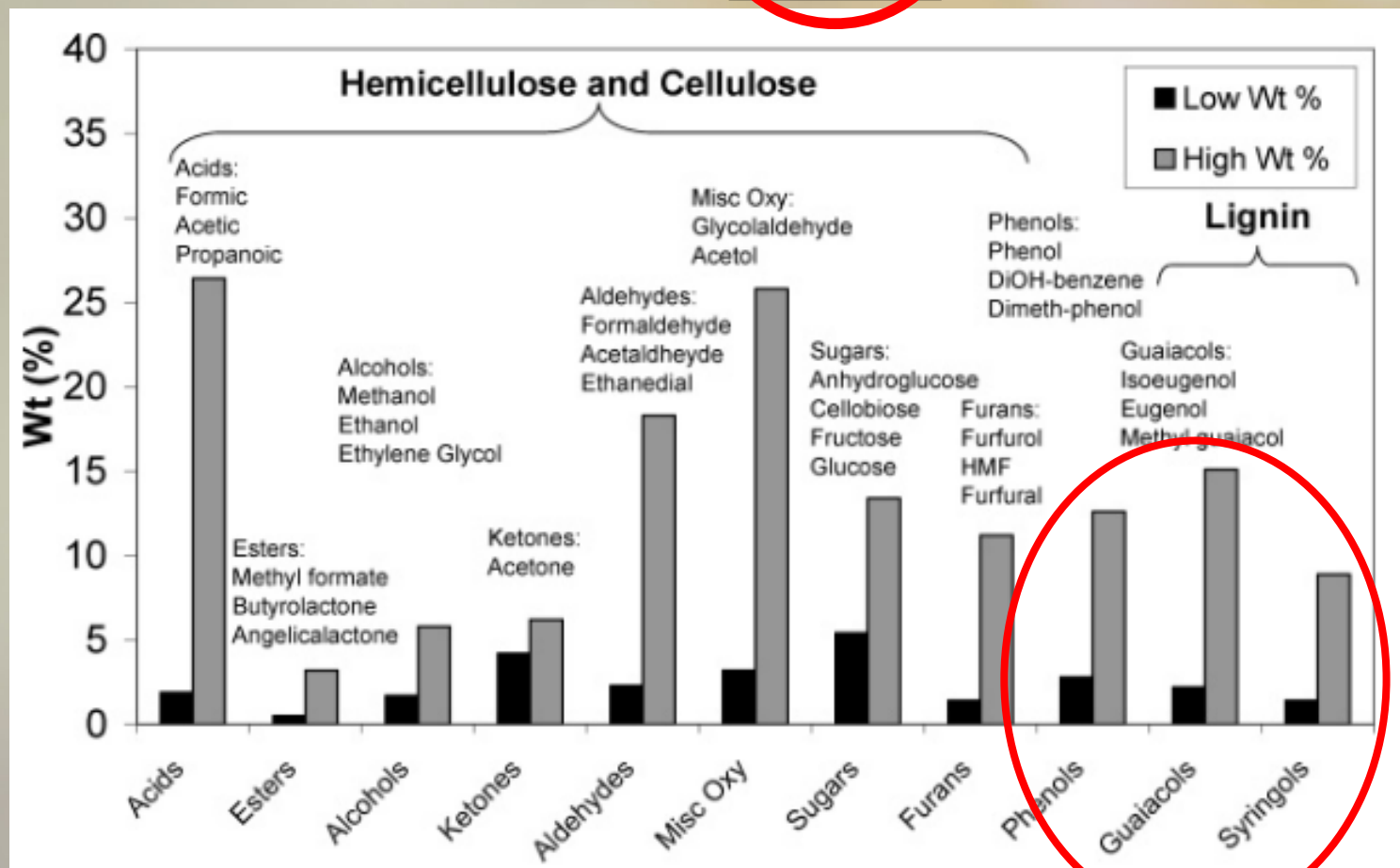
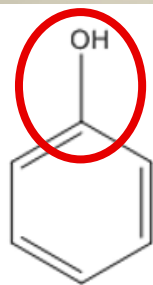


Photo by Dennis Schroeder, NREL 20404.

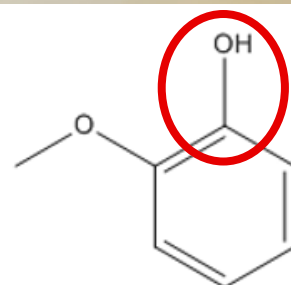
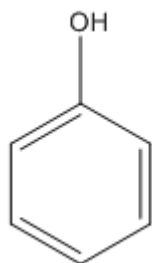


Chemical composition of bio-oil <sup>1</sup>, as summarized in <sup>2</sup>

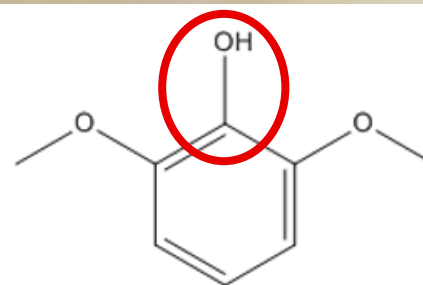
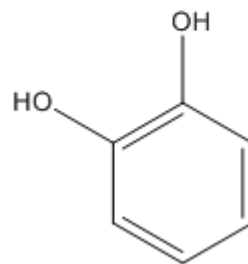
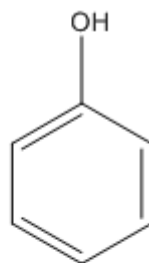
## Toughest Deoxygenation: the phenolic C-O bond



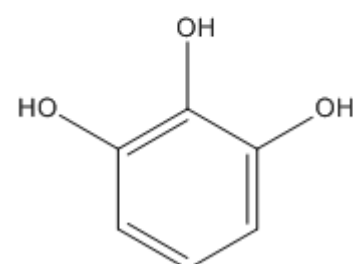
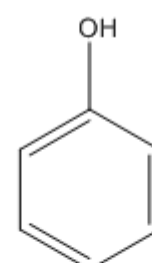
phenol



guaiacol



syringol

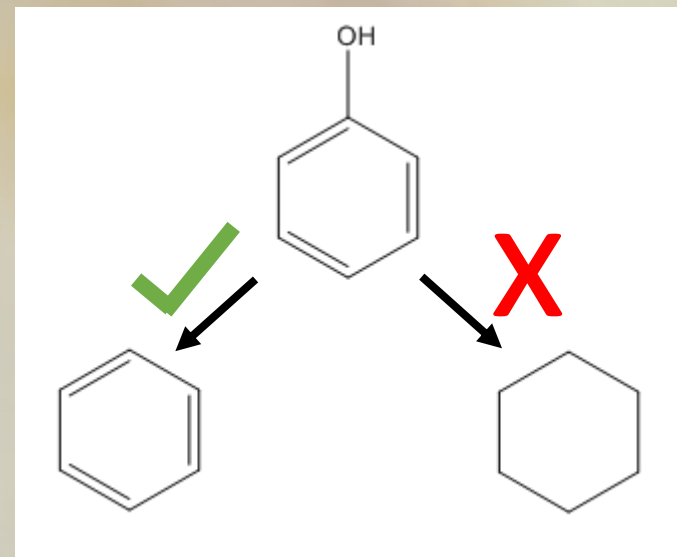




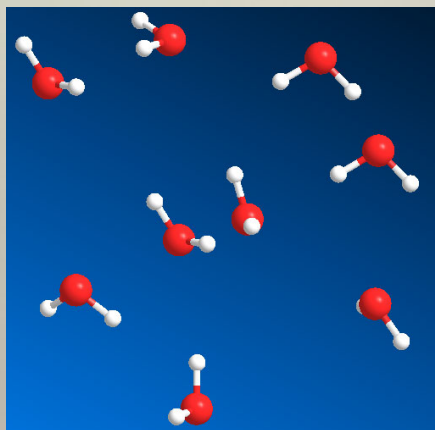
# Challenges

Additional difficulties:

- Selectively breaking C-O bond
  - Uses less hydrogen
  - Preserving aromaticity keeps octane value high



- Water in bio-oil: deactivates catalysts by oxidation



# Potential Solution: Pd-Fe

Why Pd-Fe? For gas phase HDO:

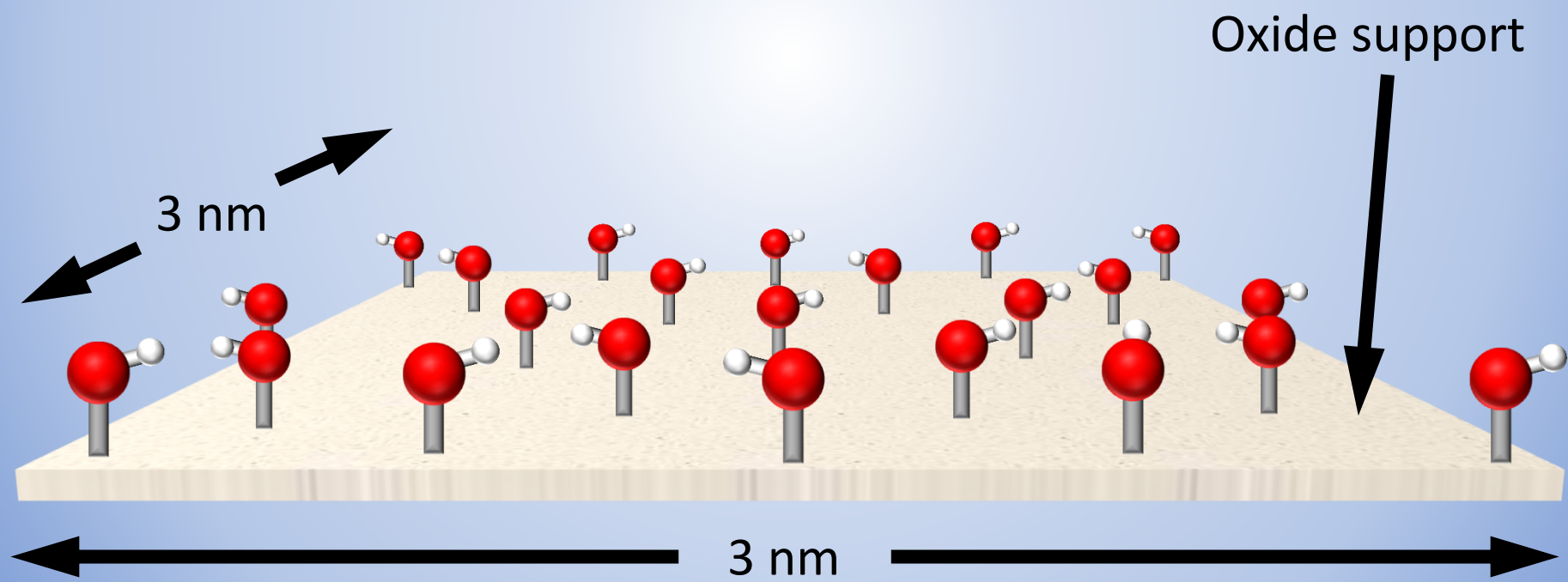
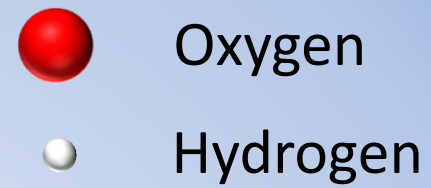
- Fe<sup>0</sup> has high selectivity, but low activity and quick deactivation by water<sup>3,4</sup>
- Pd has low selectivity, but high activity and stability<sup>5</sup>
- Synergistic effect gives high selectivity and activity<sup>6,7,8</sup>
- Pd also stabilizes Fe against deactivation<sup>9,10</sup>

## Hypothesis

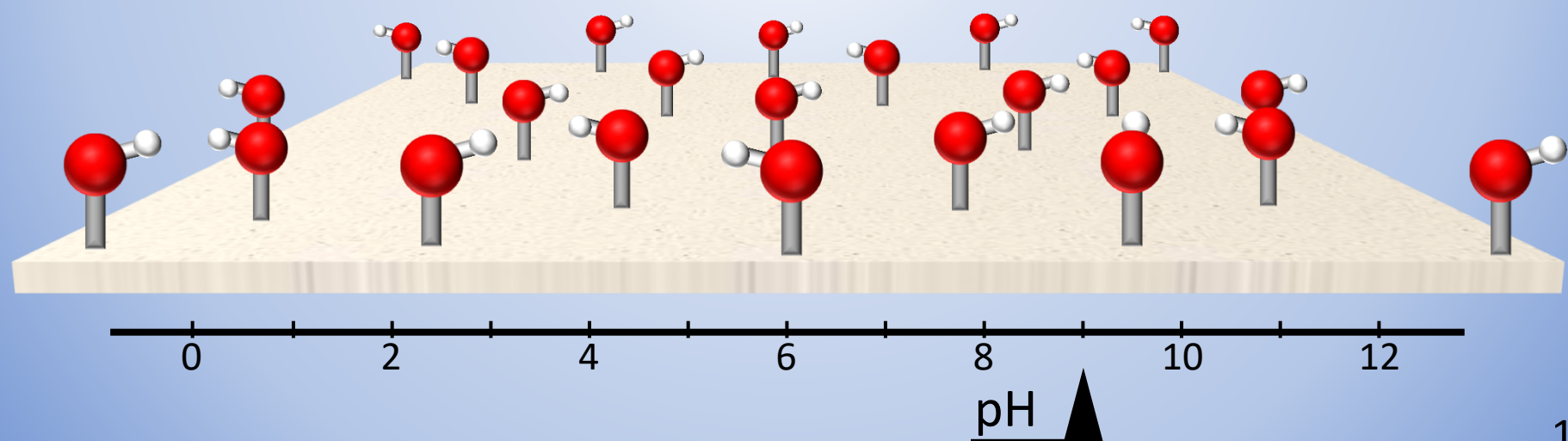
Pd-Fe catalysts with a higher Fe utilization and better stability against water oxidation (via a more thorough Pd-Fe interaction) might be achieved by depositing Pd selectively onto supported iron oxide particles using SEA prior to reduction

# Strong Electrostatic Adsorption (SEA)

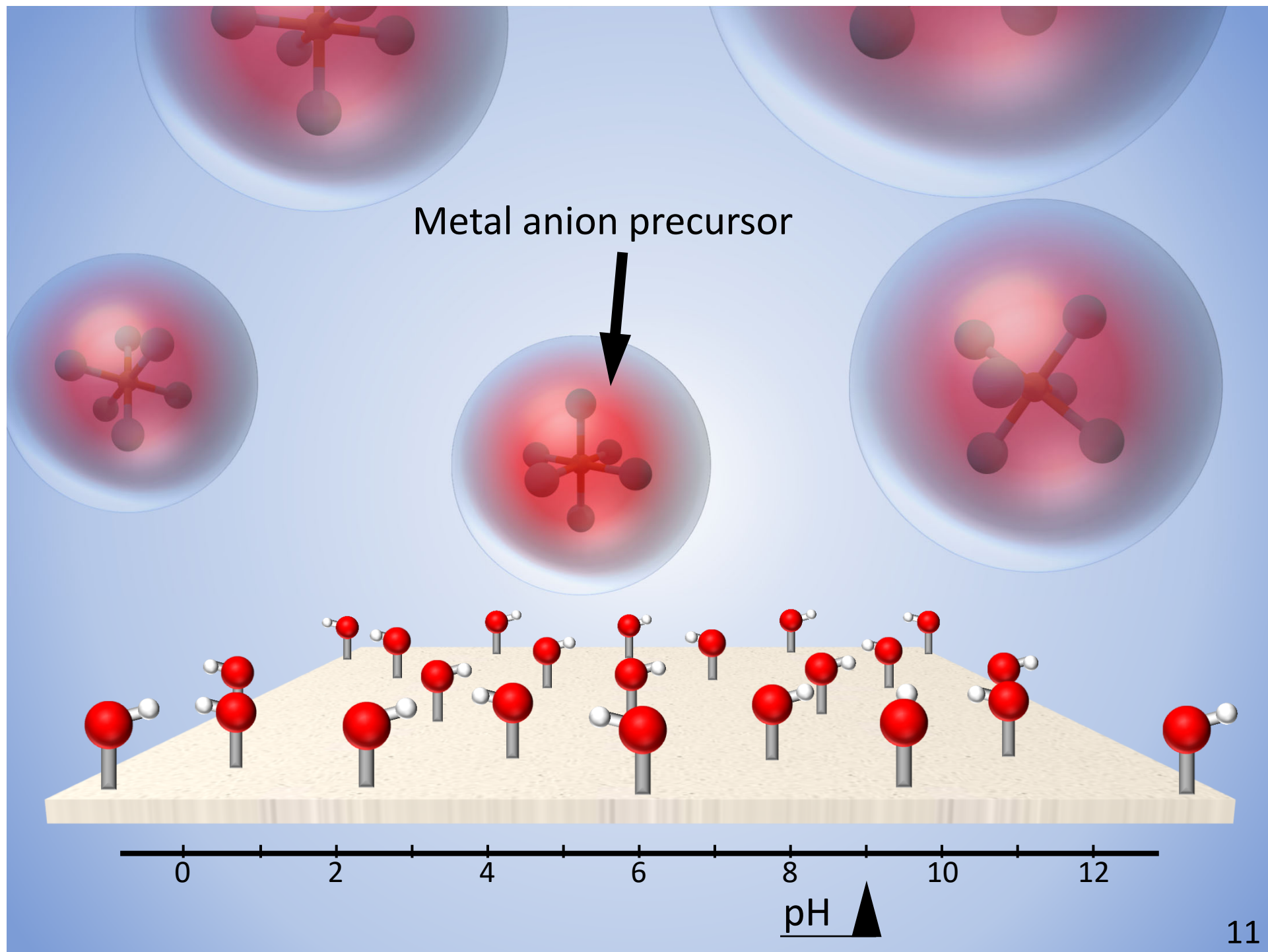


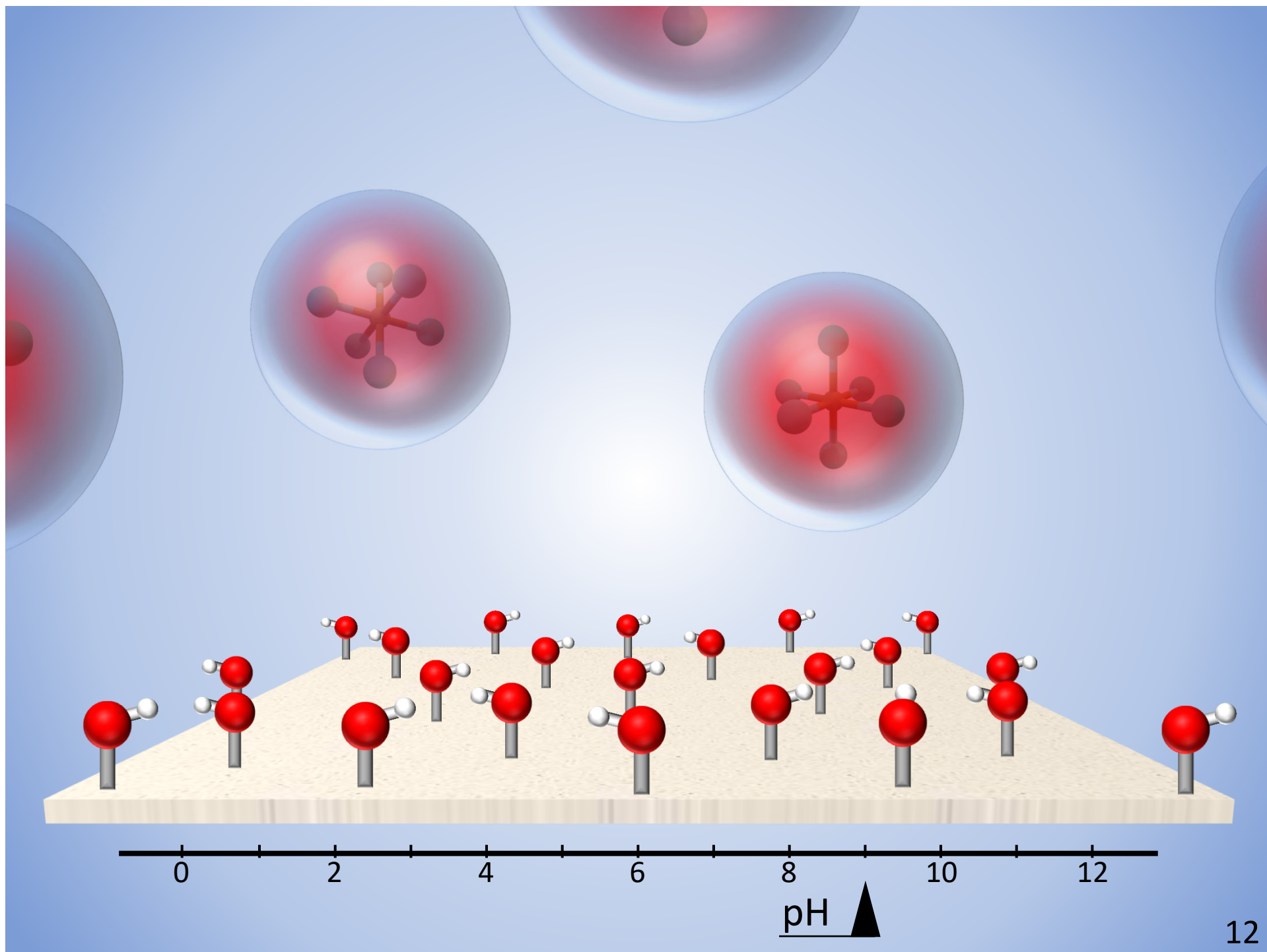


## Point of Zero Charge (PZC)



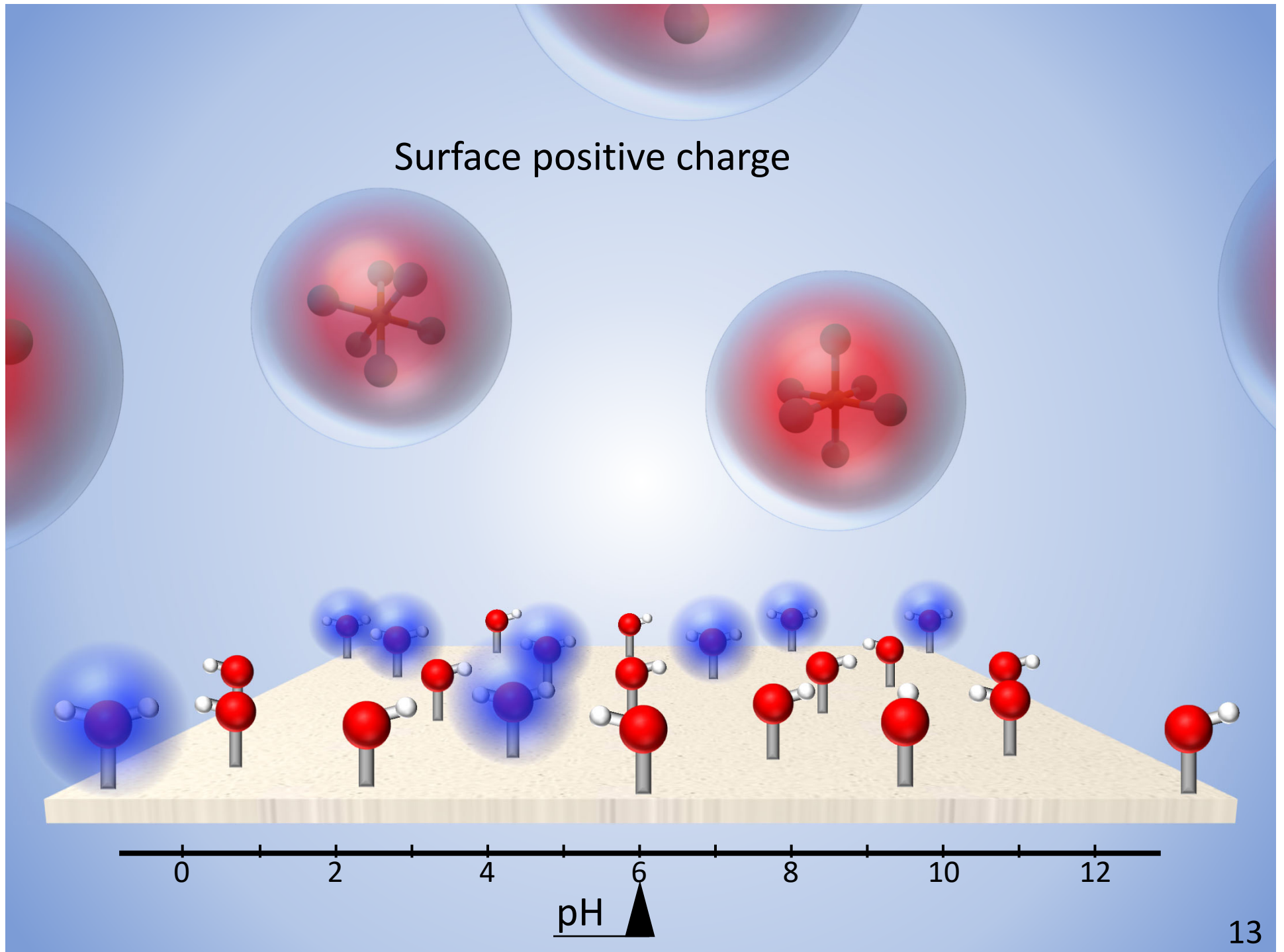
Metal anion precursor





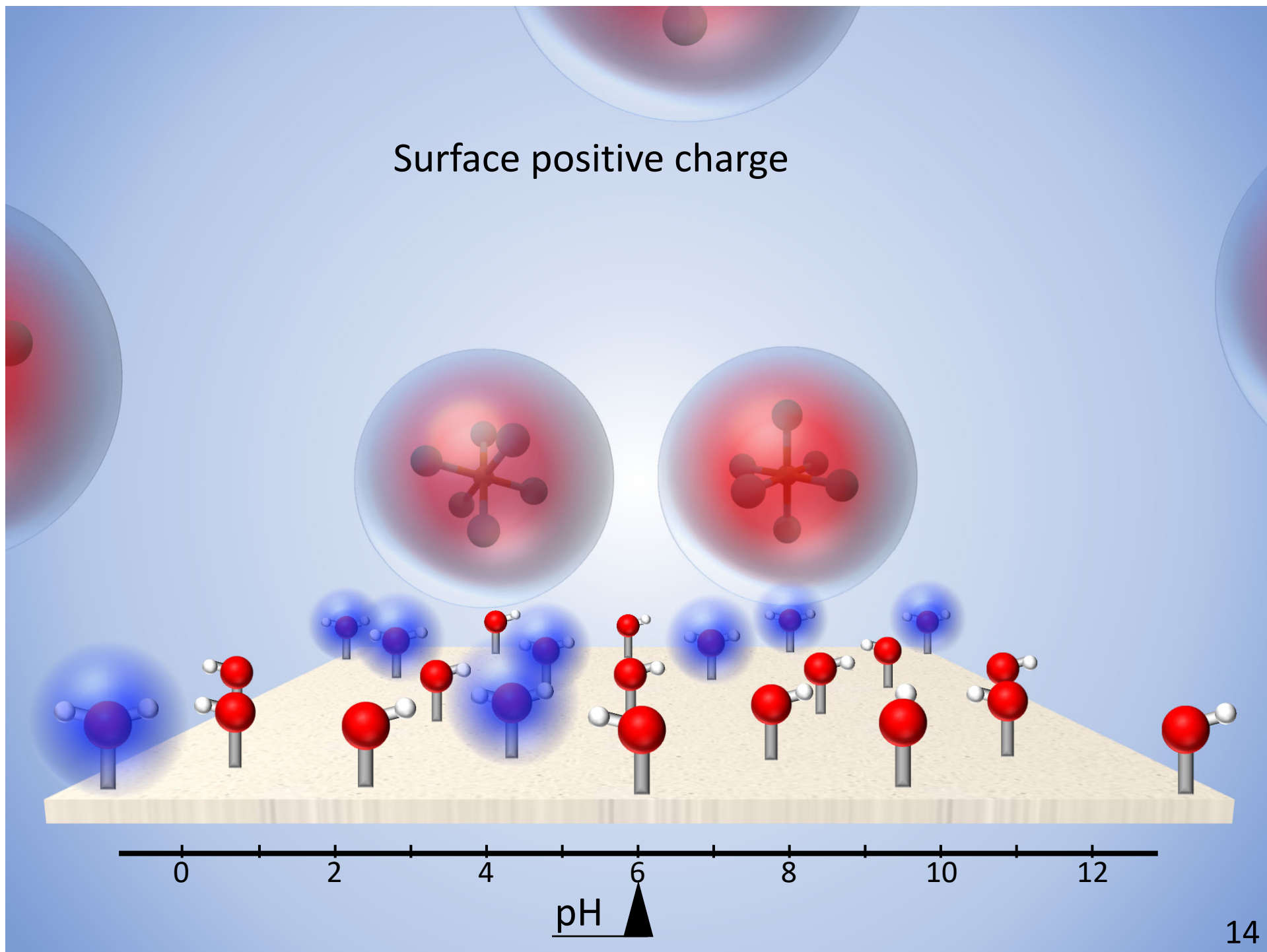


Surface positive charge

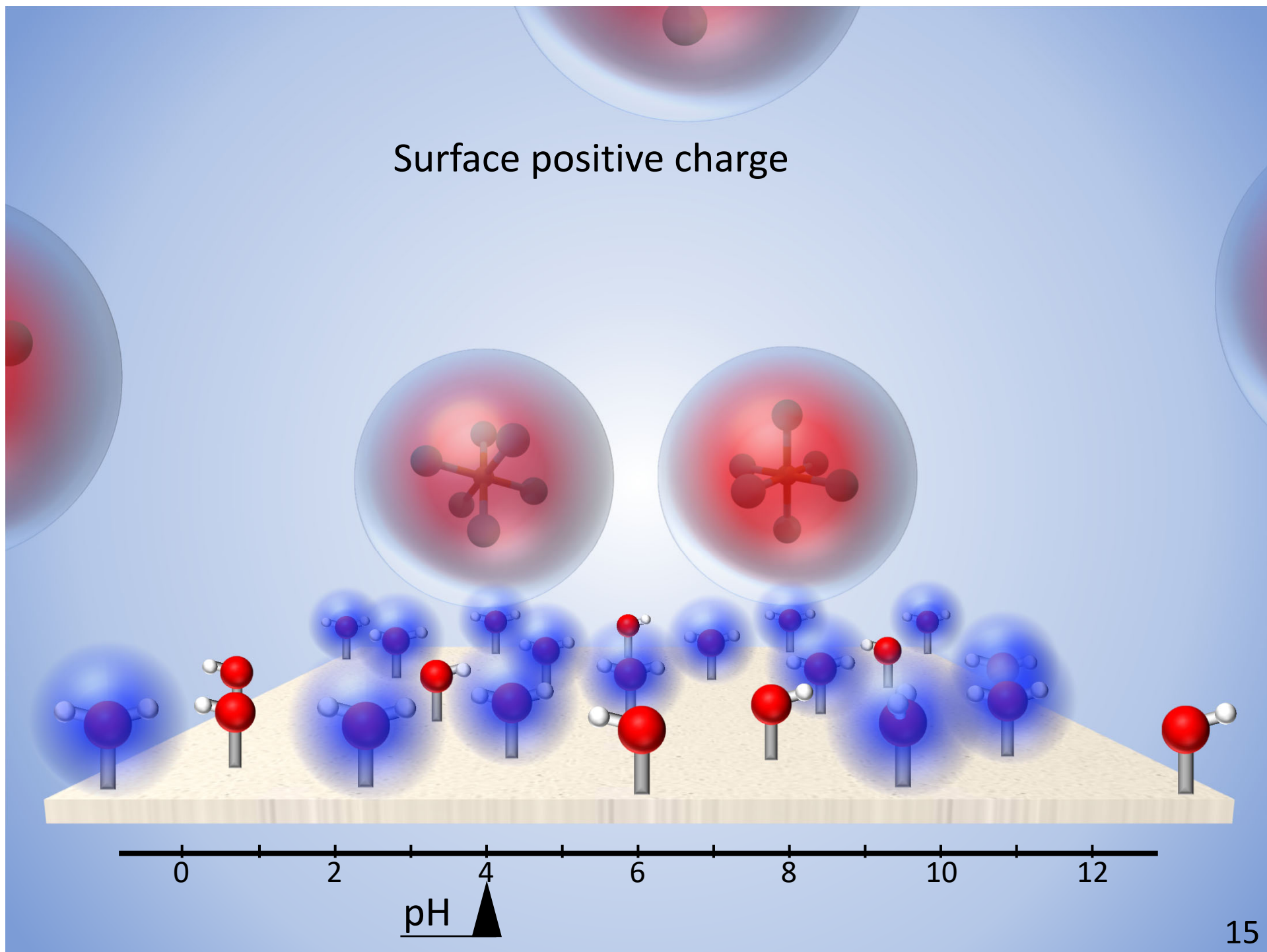




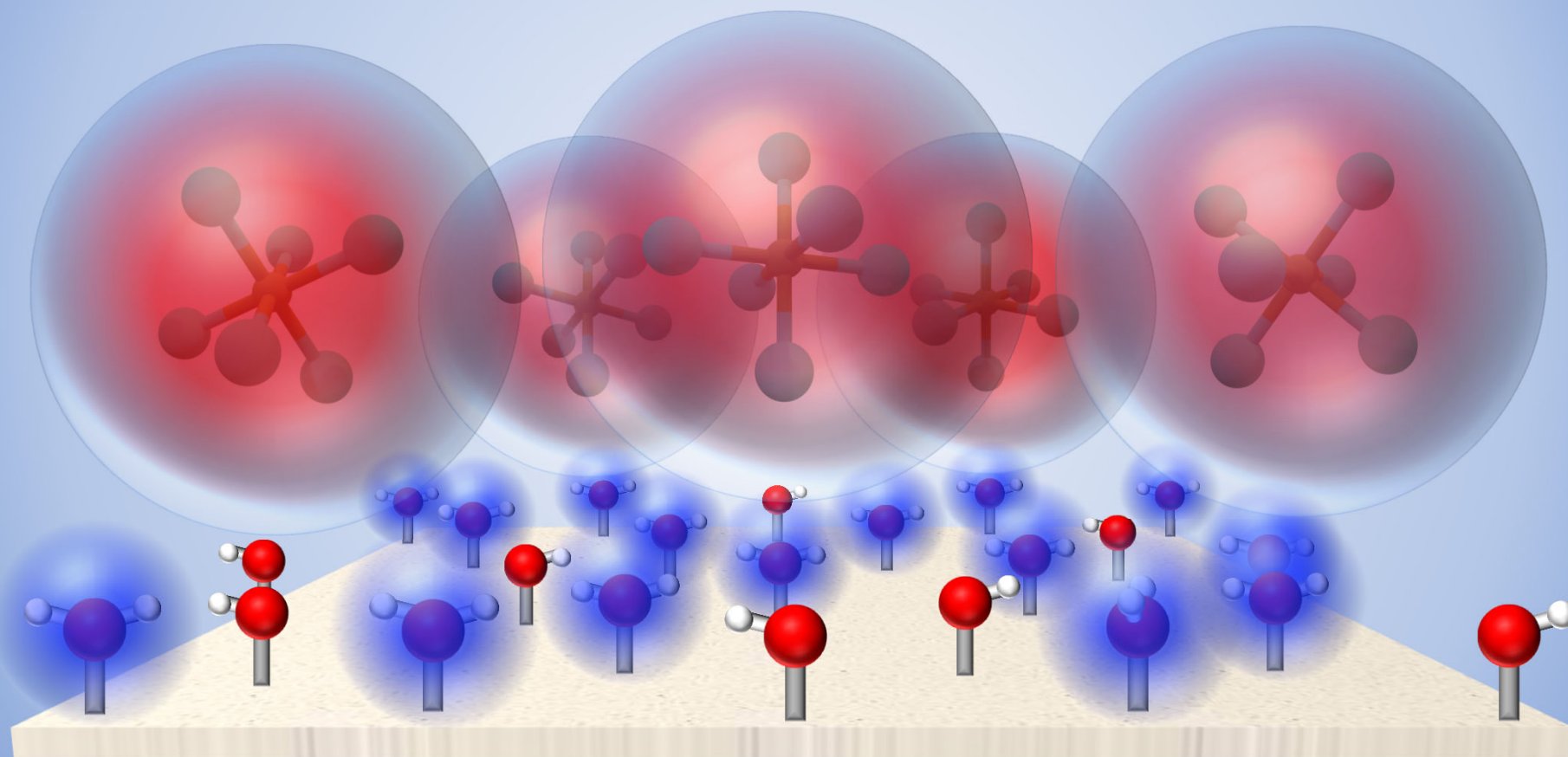
Surface positive charge



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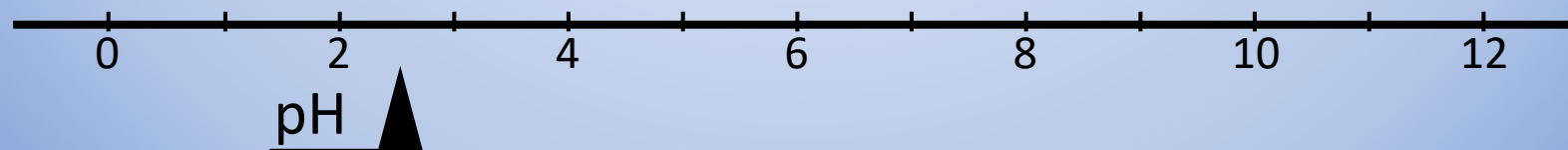
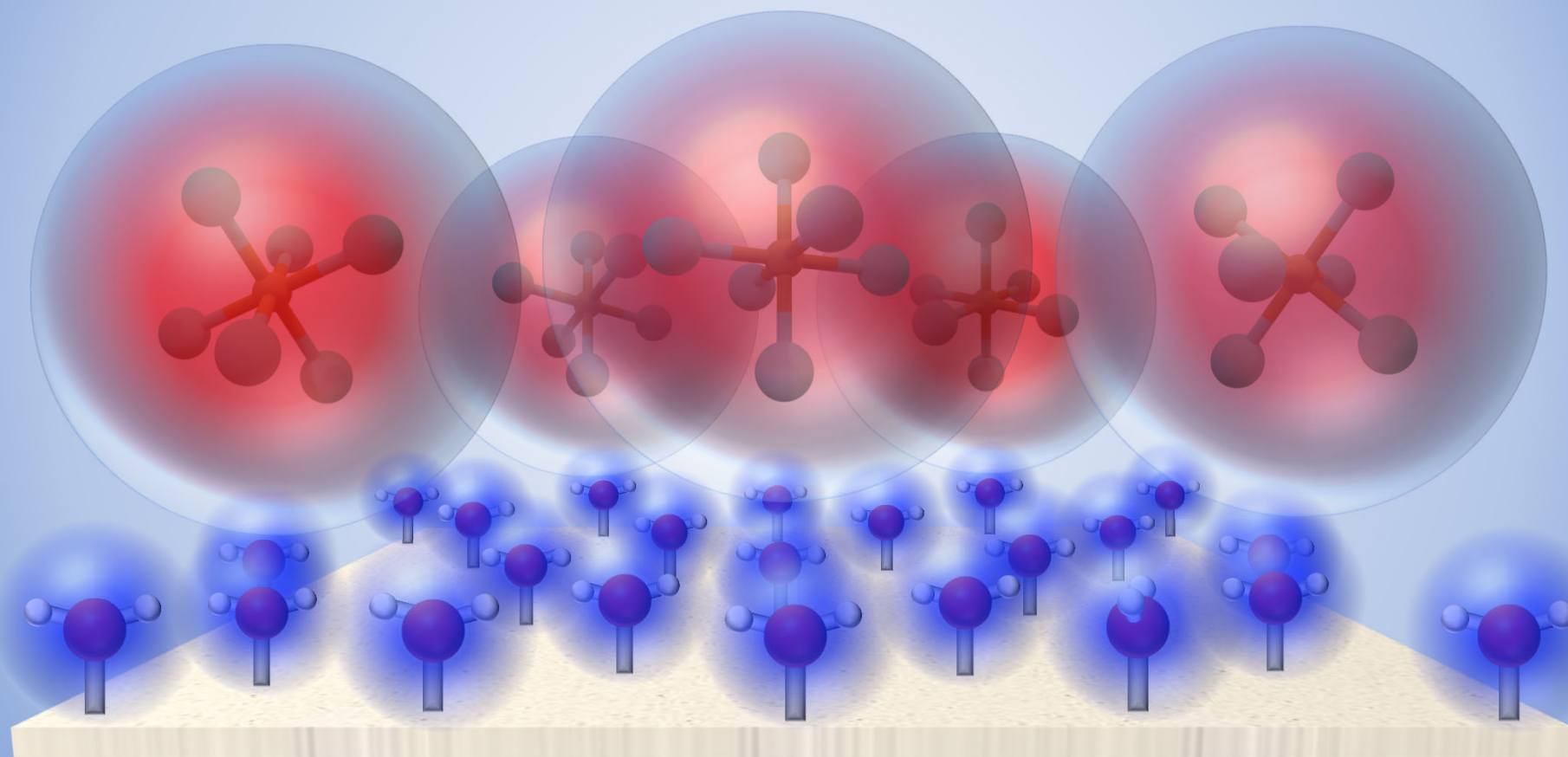


Surface positive charge





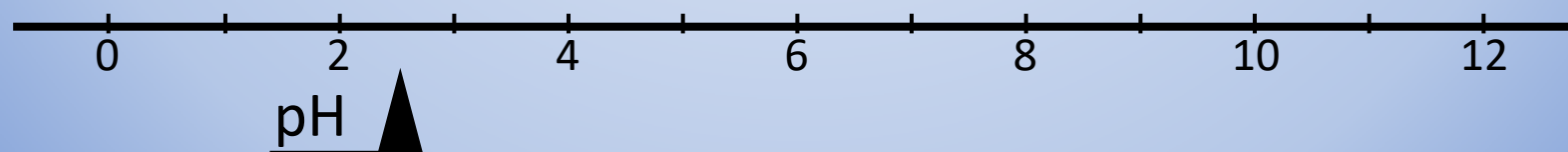
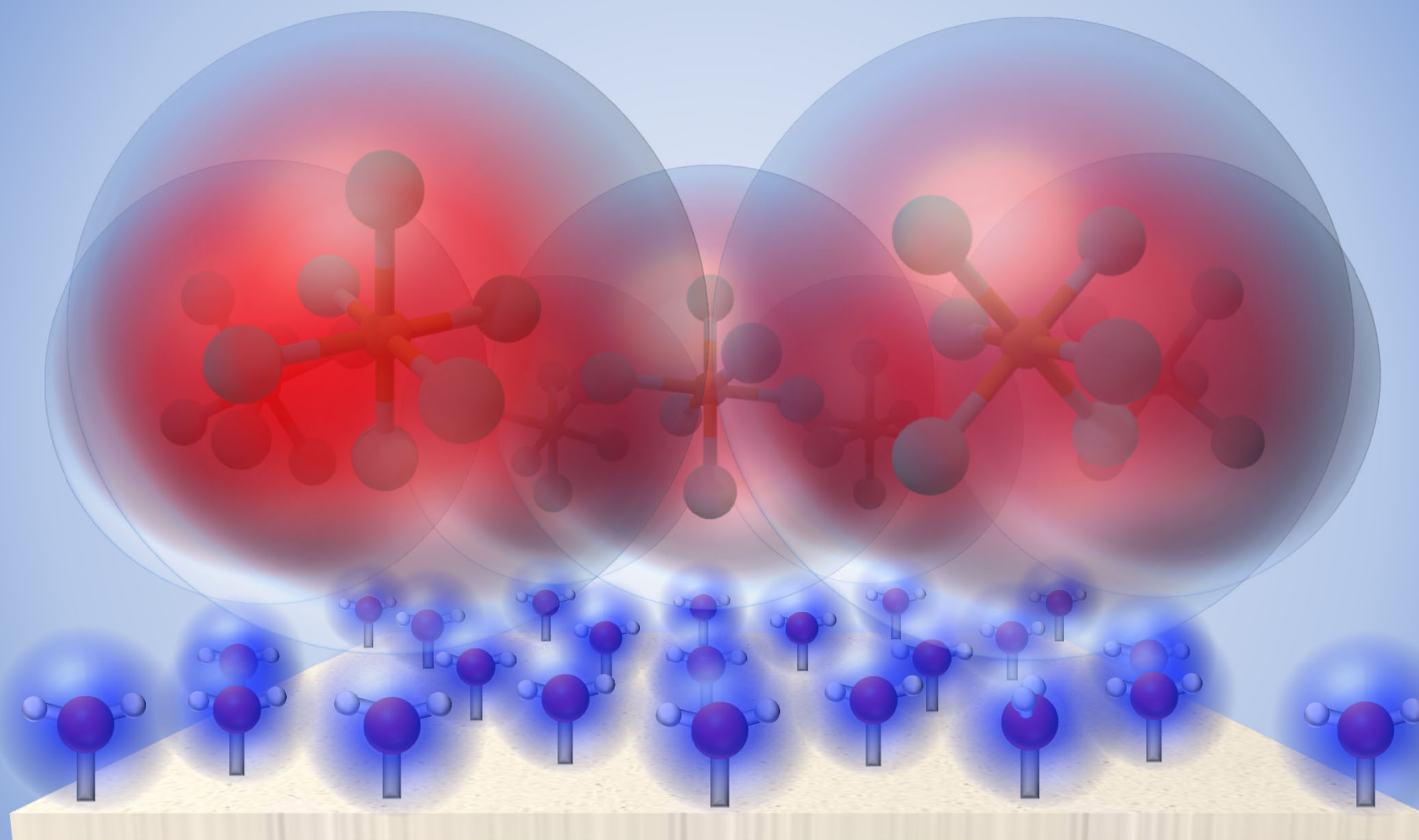
Surface positive charge







Surface positive charge



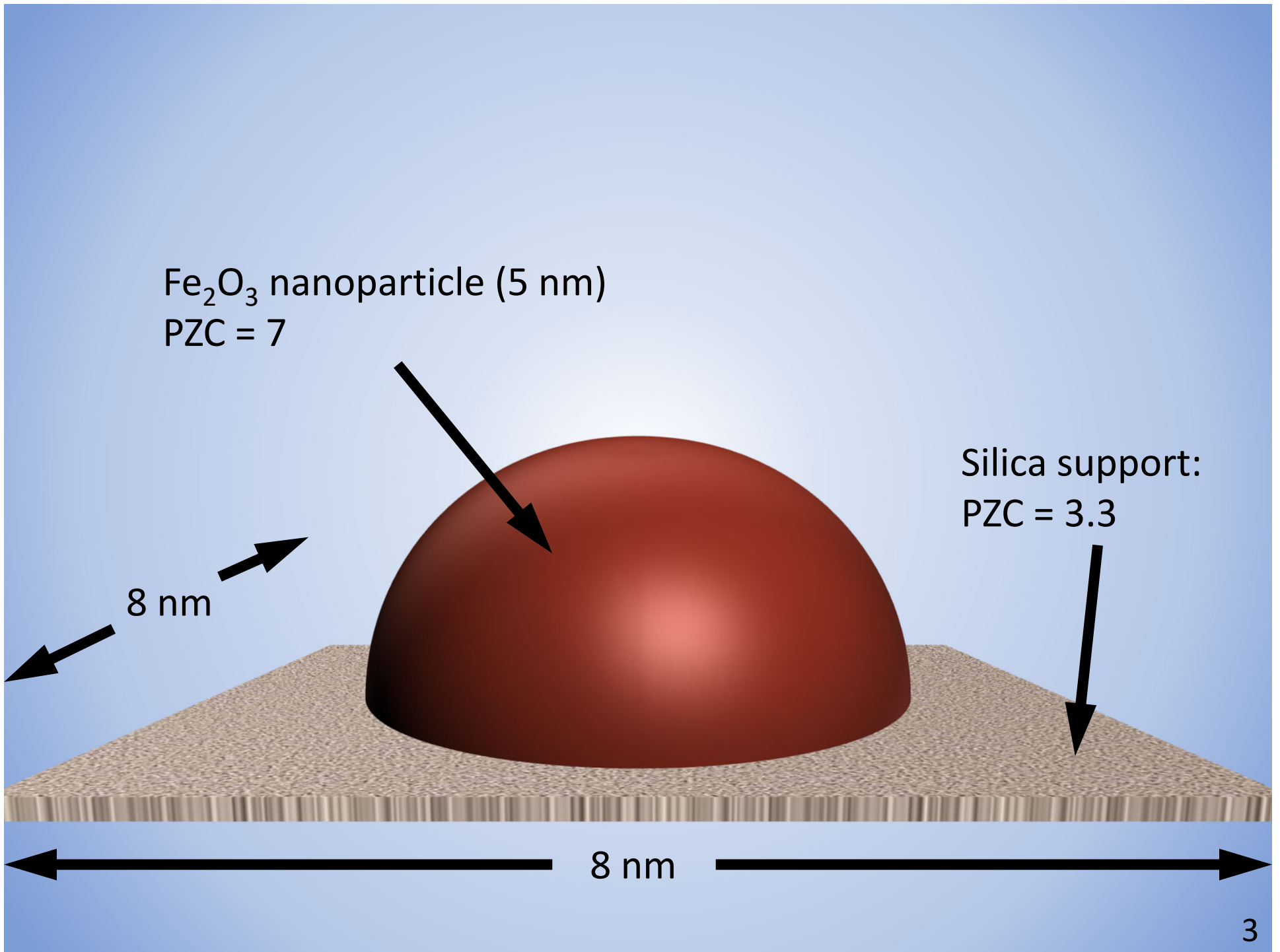
# SEA on silica-supported $\text{Fe}_2\text{O}_3$

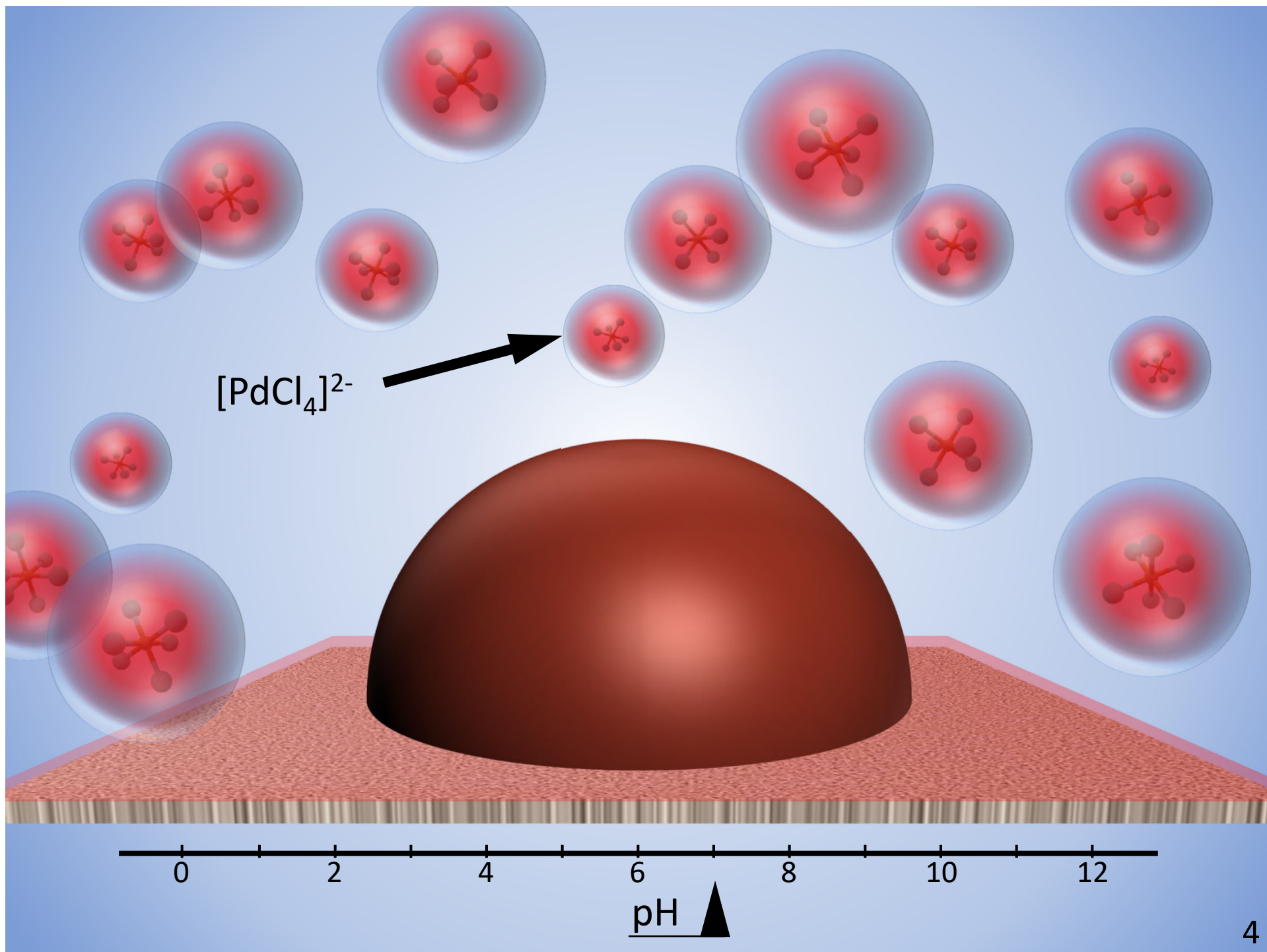
$\text{Fe}_2\text{O}_3$  nanoparticle (5 nm)  
PZC = 7

Silica support:  
PZC = 3.3

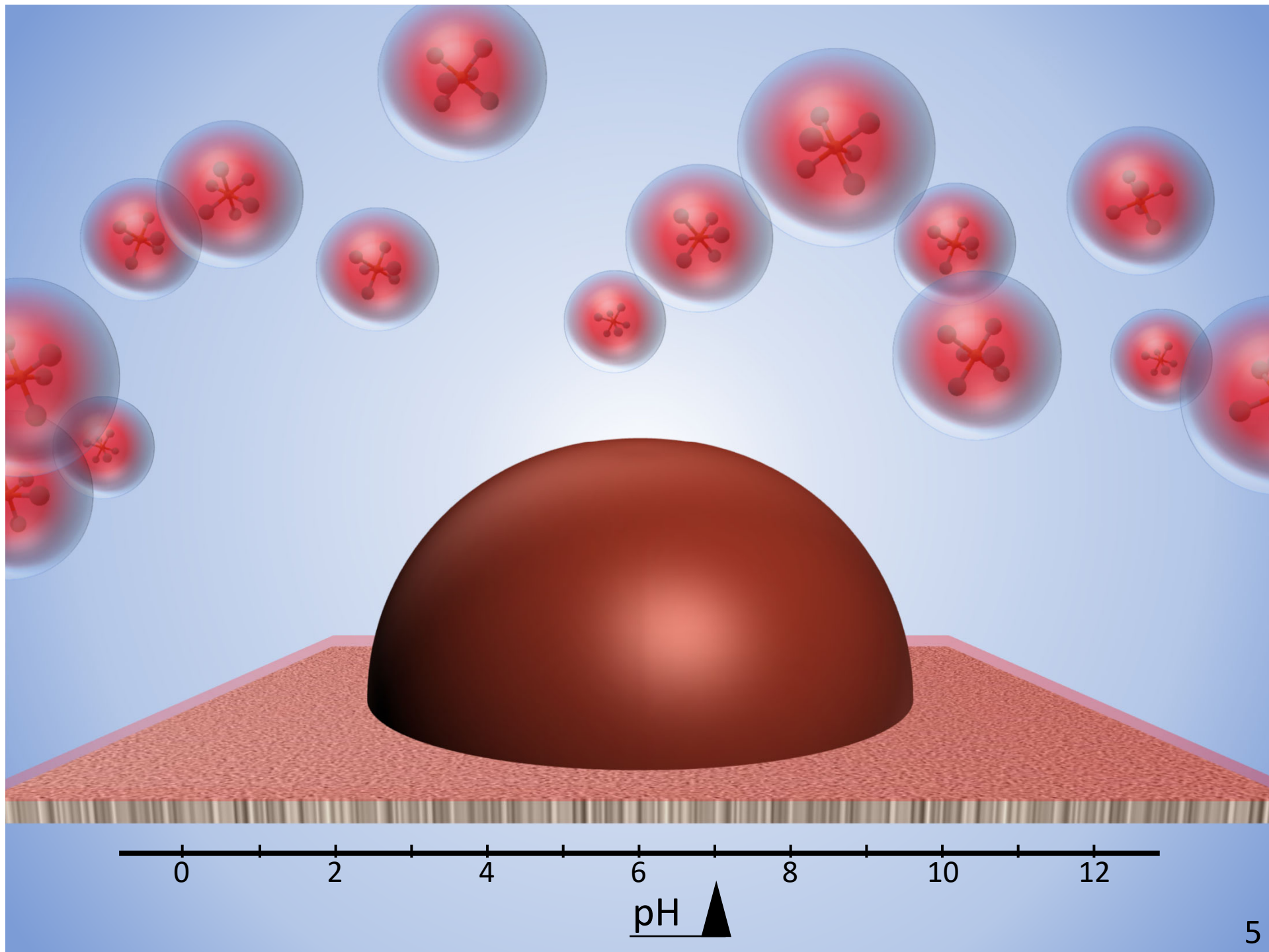
8 nm

8 nm

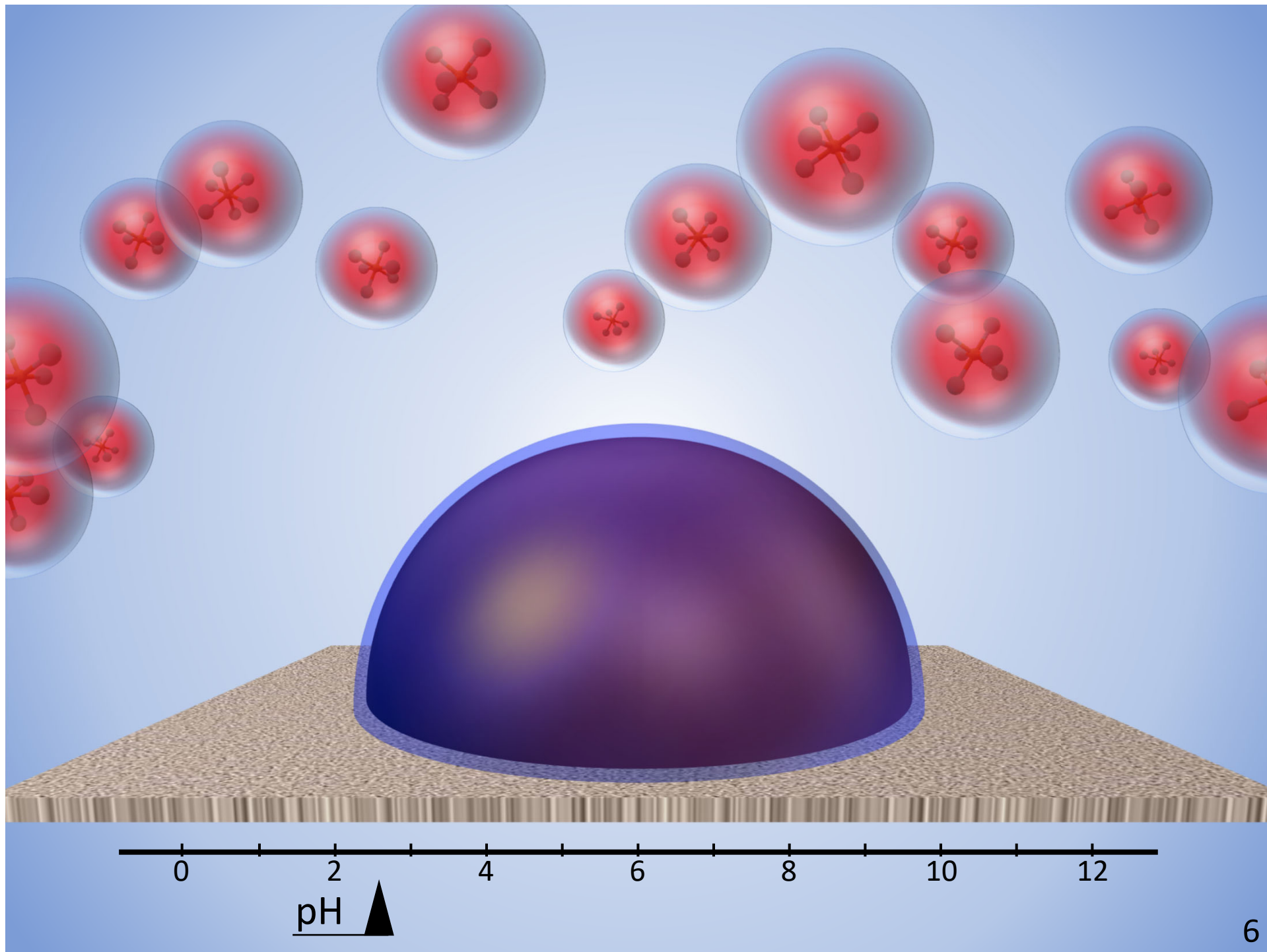


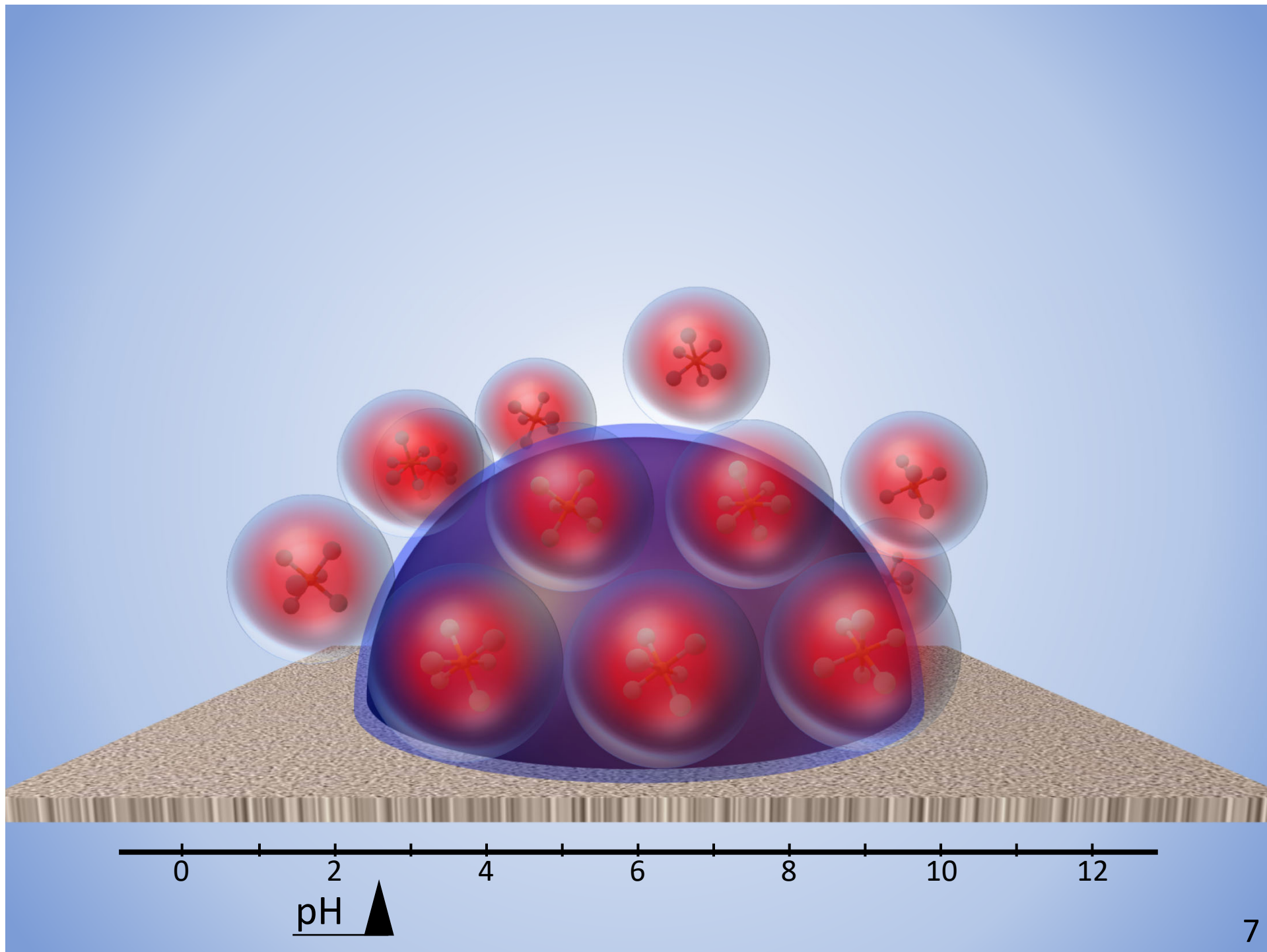












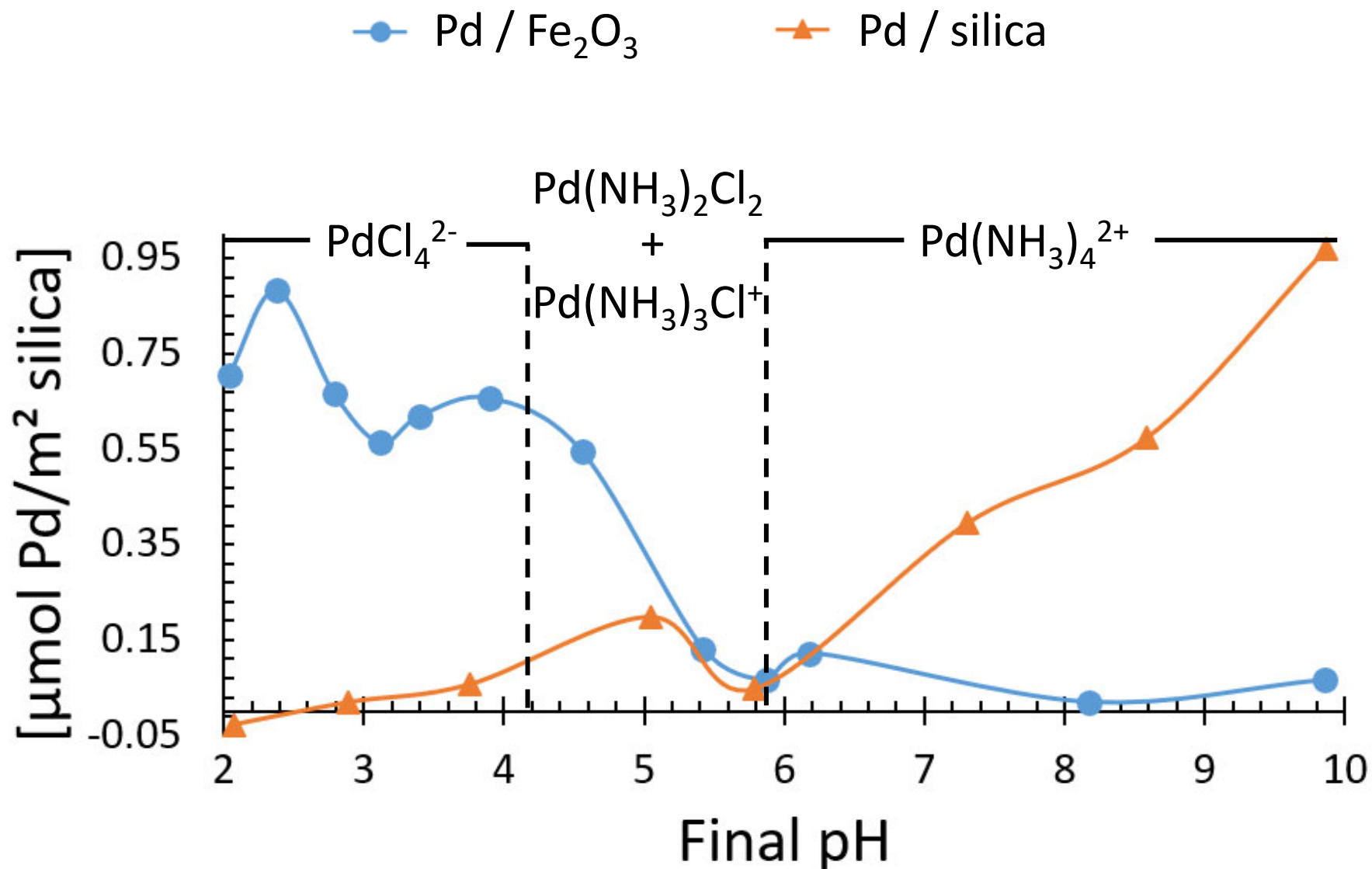
# Synthesis and Characterization

# Synthesis and Characterization

Question	Technique used to answer
What pH values to use for SEA synthesis?	Uptake Survey using Inductively Coupled Plasma Optical Emission Spectroscopy (ICP-OES)
What is the weight loading of the Pd?	ICP-OES
How much interaction between Pd and Fe?	Temperature Programmed Reduction (TPR)
What crystallite phases are present?	X-ray Diffraction
What are the crystallite sizes of each phase?	X-ray Diffraction



# Uptake Survey results: Use pH 2.5



\*Pd speciation from reference 11

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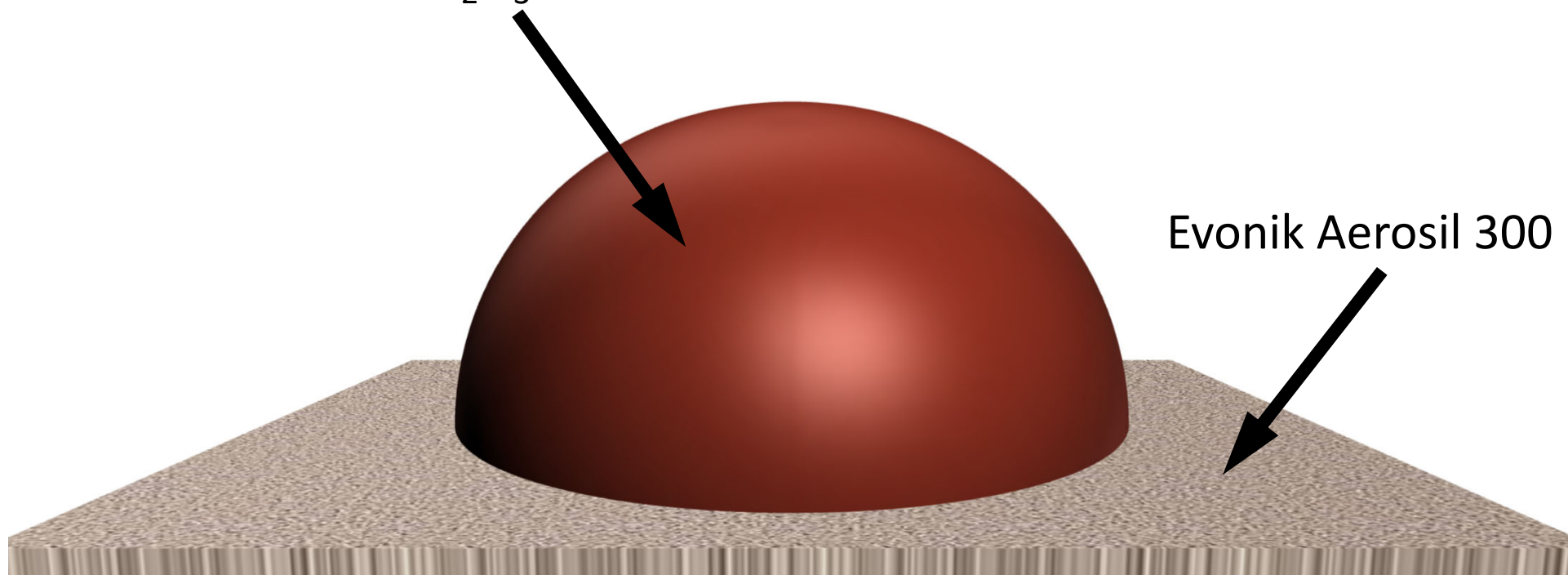
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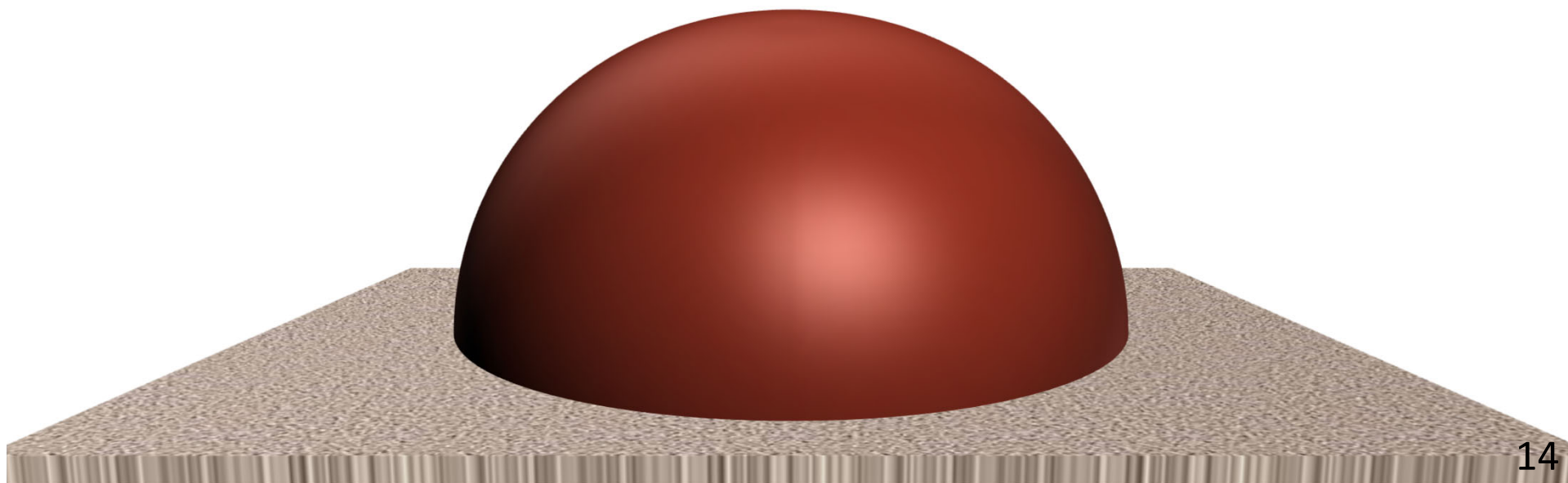
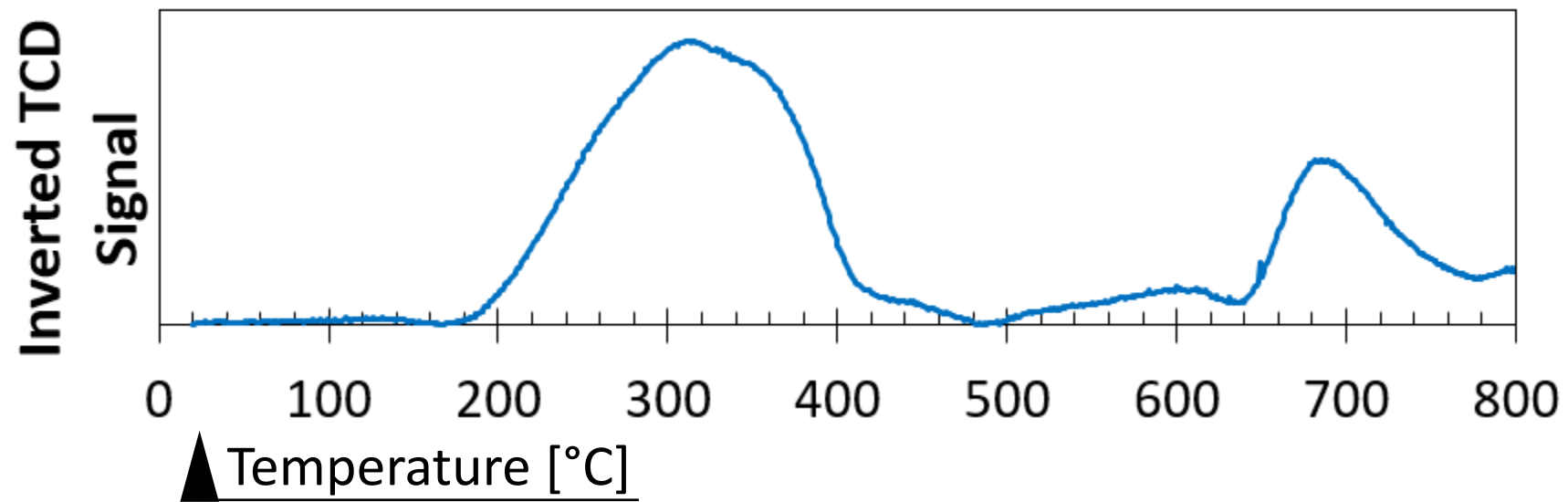
# Temperature Programmed Reduction (TPR)

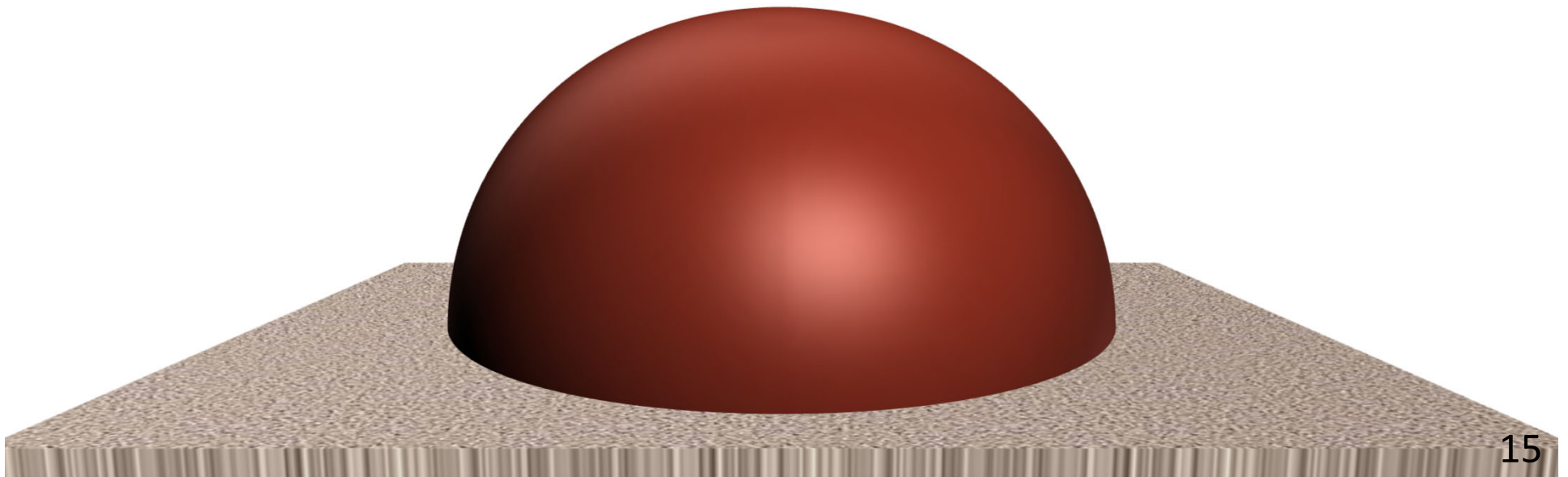
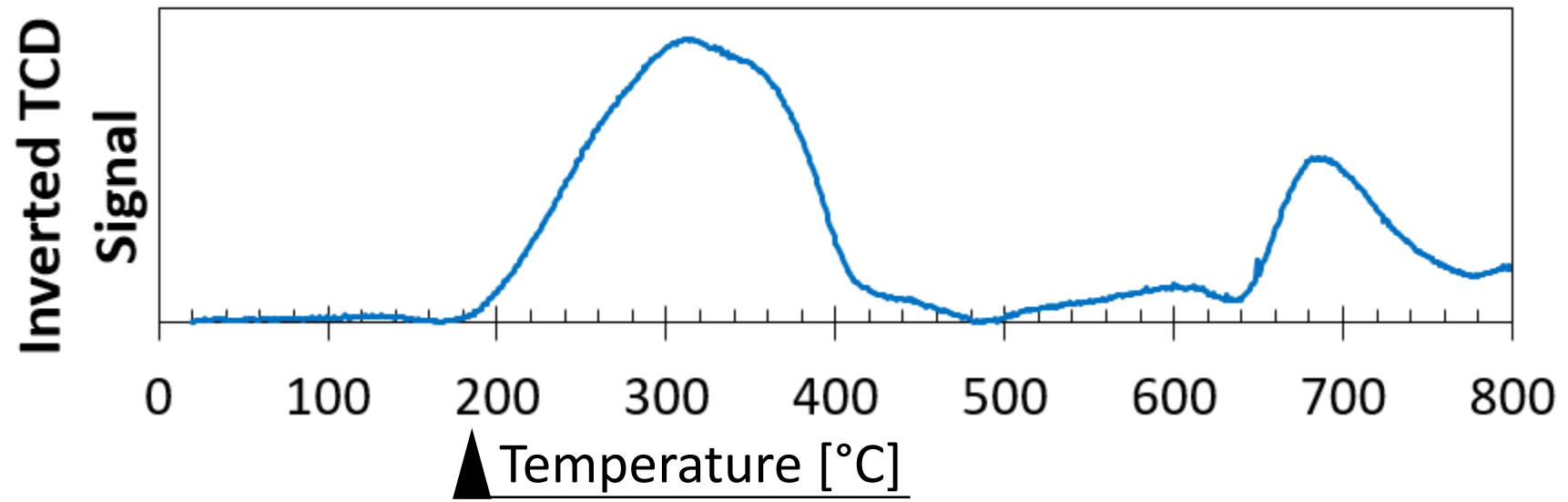
Conditions: 10 °C / min, 50 sccm 10% H<sub>2</sub> in Ar

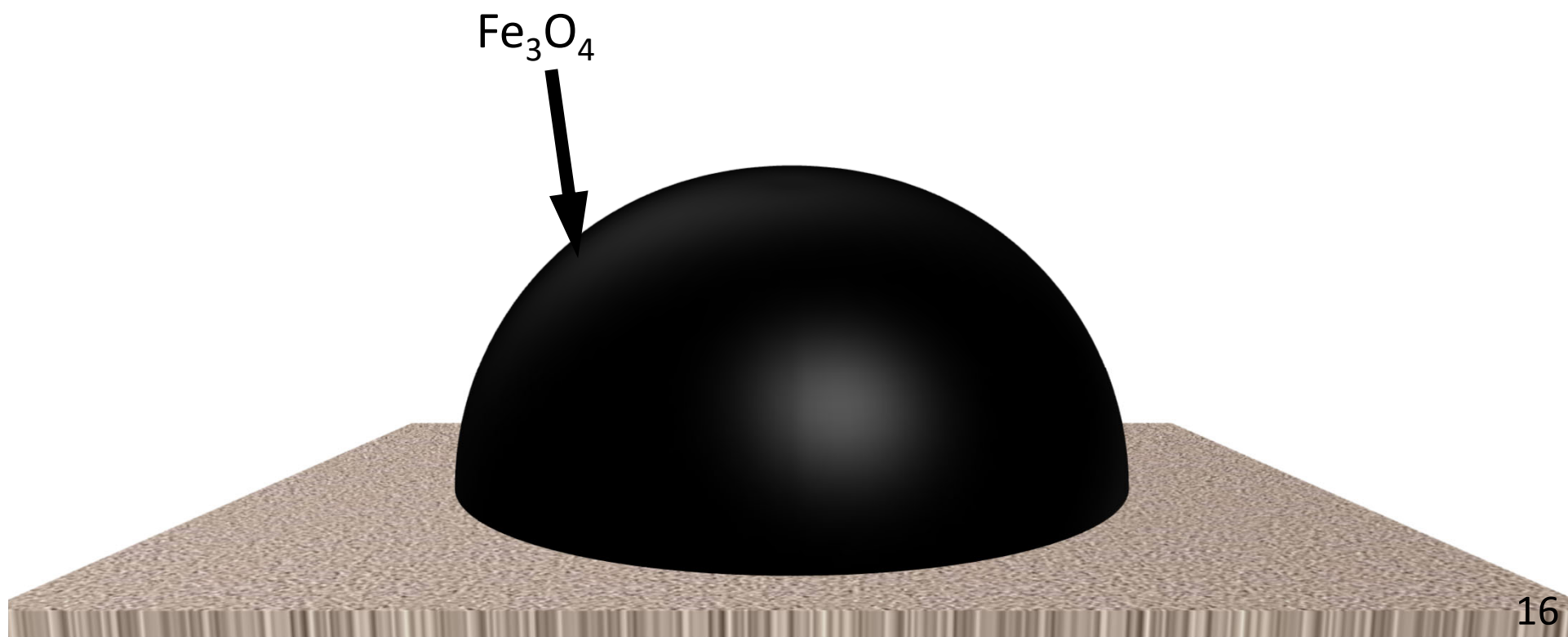
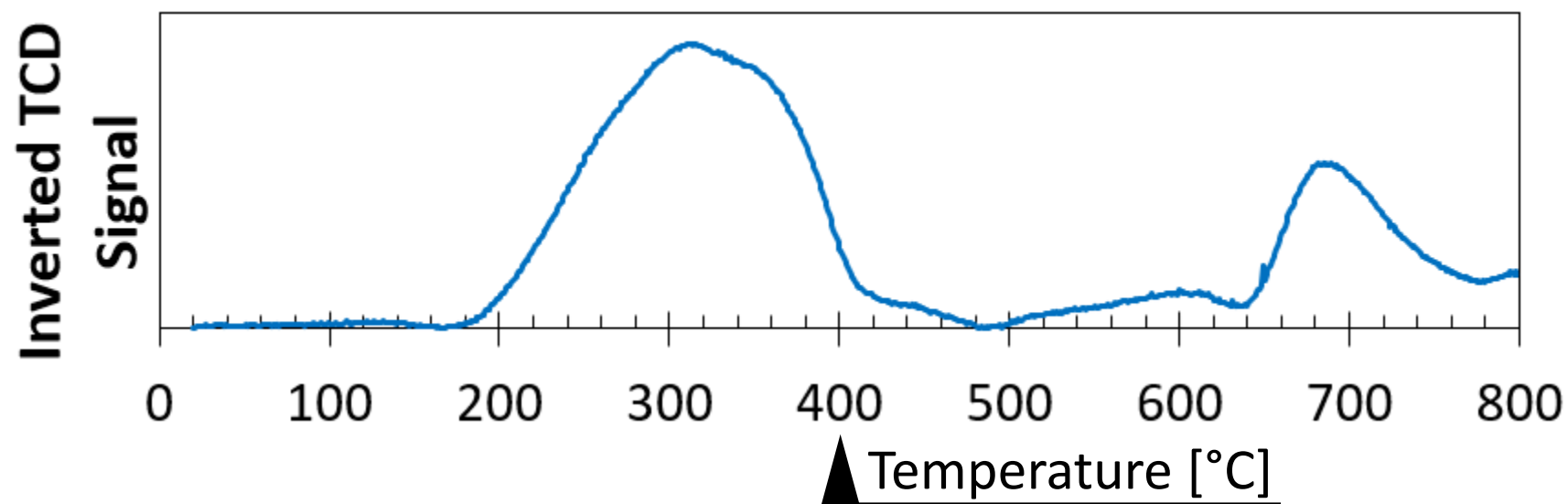
Fe<sub>2</sub>O<sub>3</sub> nanoparticle (5 nm)  
13.3 wt% Fe<sub>2</sub>O<sub>3</sub> (9.7 wt% Fe)

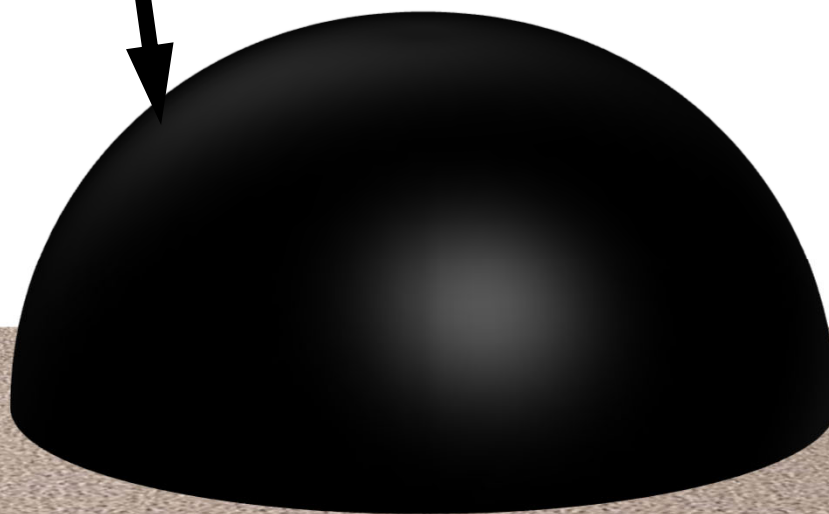
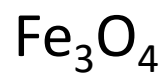
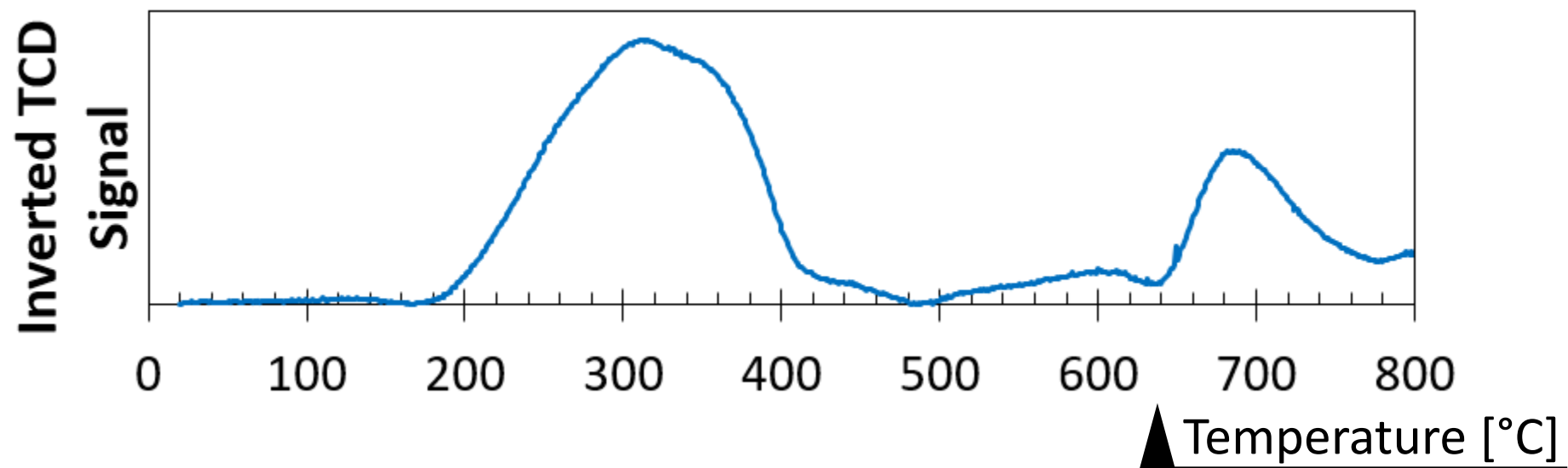




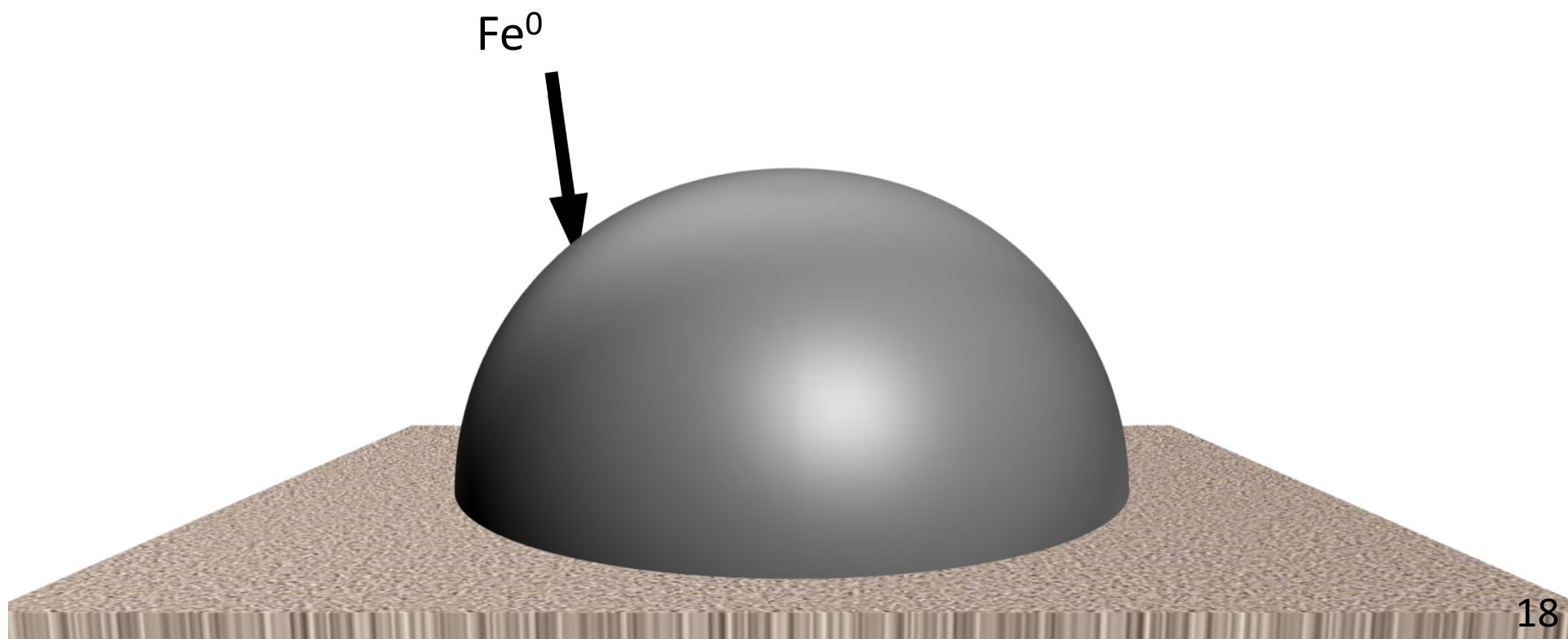
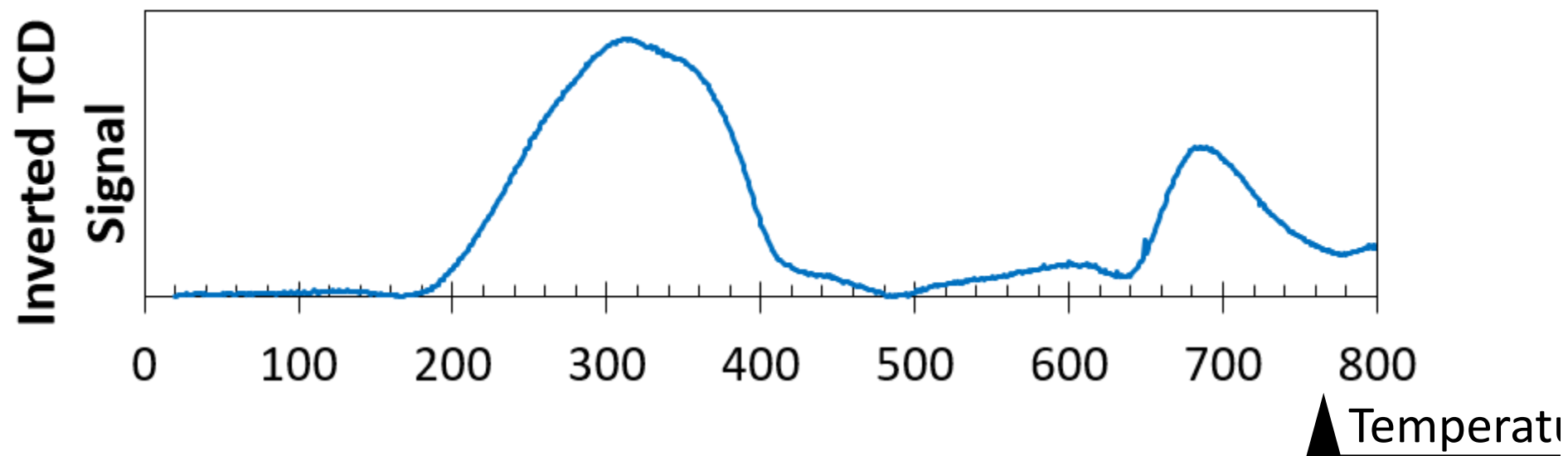




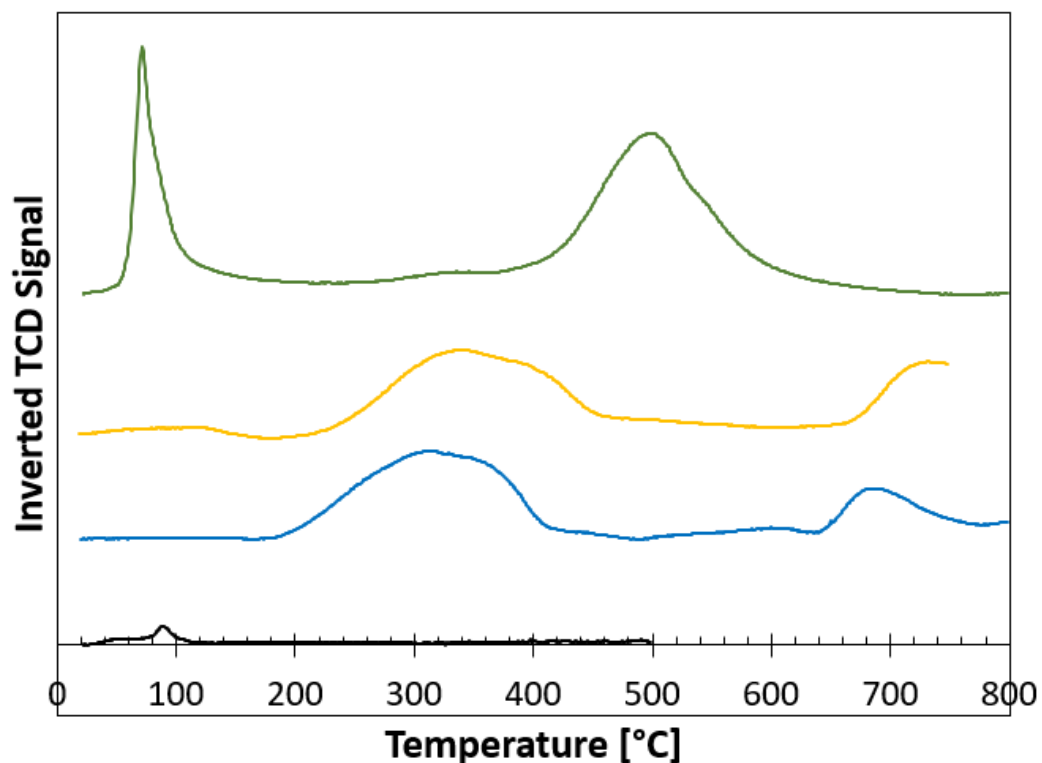








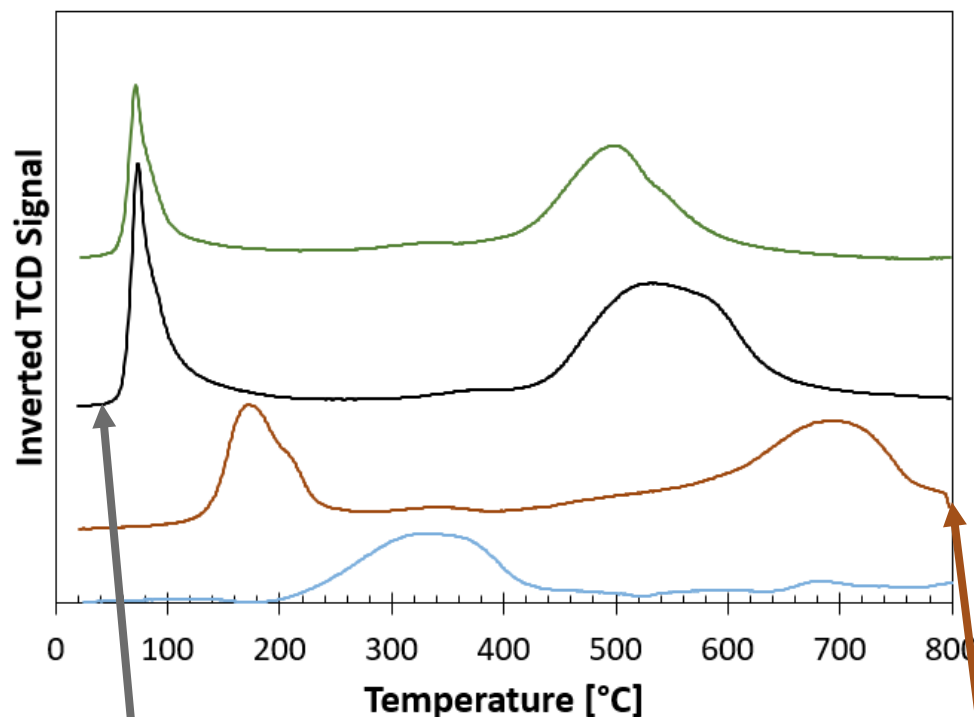
# Pd-Fe interaction: TPR



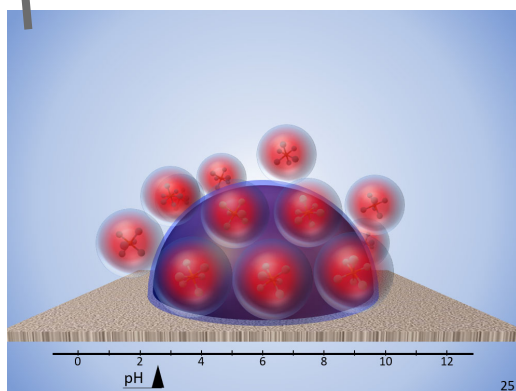
Sample	Pd [mg]	Fe <sub>2</sub> O <sub>3</sub> [mg]
0.17%Pd / 13.7%Fe <sub>2</sub> O <sub>3</sub> / A300	0.35	28.0
13.7%Fe <sub>2</sub> O <sub>3</sub> / A300 + 1.8%Pd / A300	0.35	27.2
13.7%Fe <sub>2</sub> O <sub>3</sub> / A300	0	28.0
1.8%Pd / A300	0.35	0

- Physically mixing samples in the TPR does not aid in reduction
- SEA to put Pd on Fe<sub>2</sub>O<sub>3</sub> greatly aids reduction

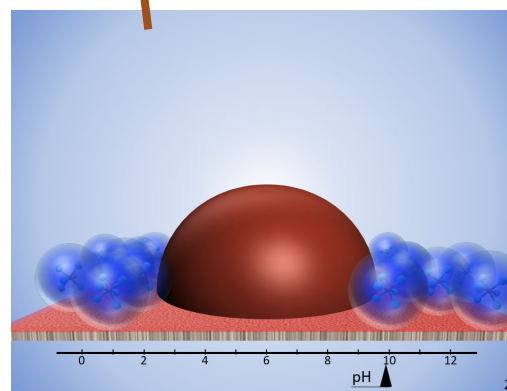
# H<sub>2</sub> Spillover vs. Pd proximity



Sample	Pd [mg]	Fe <sub>2</sub> O <sub>3</sub> [mg]
0.17%Pd / 13.7%Fe <sub>2</sub> O <sub>3</sub> / A300 (8 nm)	0.35	28.0
0.24%Pd / 13.3%Fe <sub>2</sub> O <sub>3</sub> / A300 pHf <b>3.06</b>	0.48	28.0
0.23%Pd / 13.3%Fe <sub>2</sub> O <sub>3</sub> / A300 pHf <b>9.90</b>	0.46	26.4
13.3% Fe <sub>2</sub> O <sub>3</sub> / A300	0	26.3

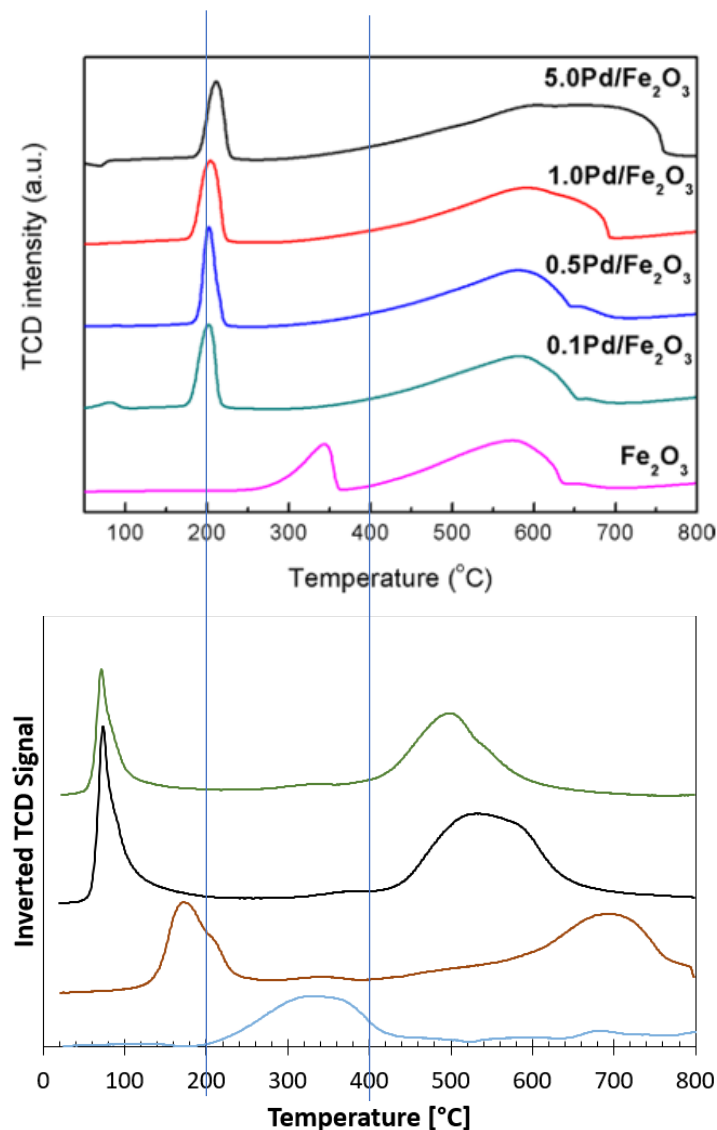


Vs.



# TPR comparison with Literature<sup>12</sup>

- SEA prepared Pd catalysts (1.72 wt% Pd on  $\text{Fe}_2\text{O}_3$ ) show the first reduction peak at 130 °C lower than 0.1 to 5wt% catalysts prepared by incipient wetness impregnation
- Evidence of stronger metal-metal interaction
- Note: the initial Fe particle sizes are different. Our silica supported  $\text{Fe}_2\text{O}_3$  particles are 5nm, their unsupported  $\text{Fe}_2\text{O}_3$  particles are 20nm.

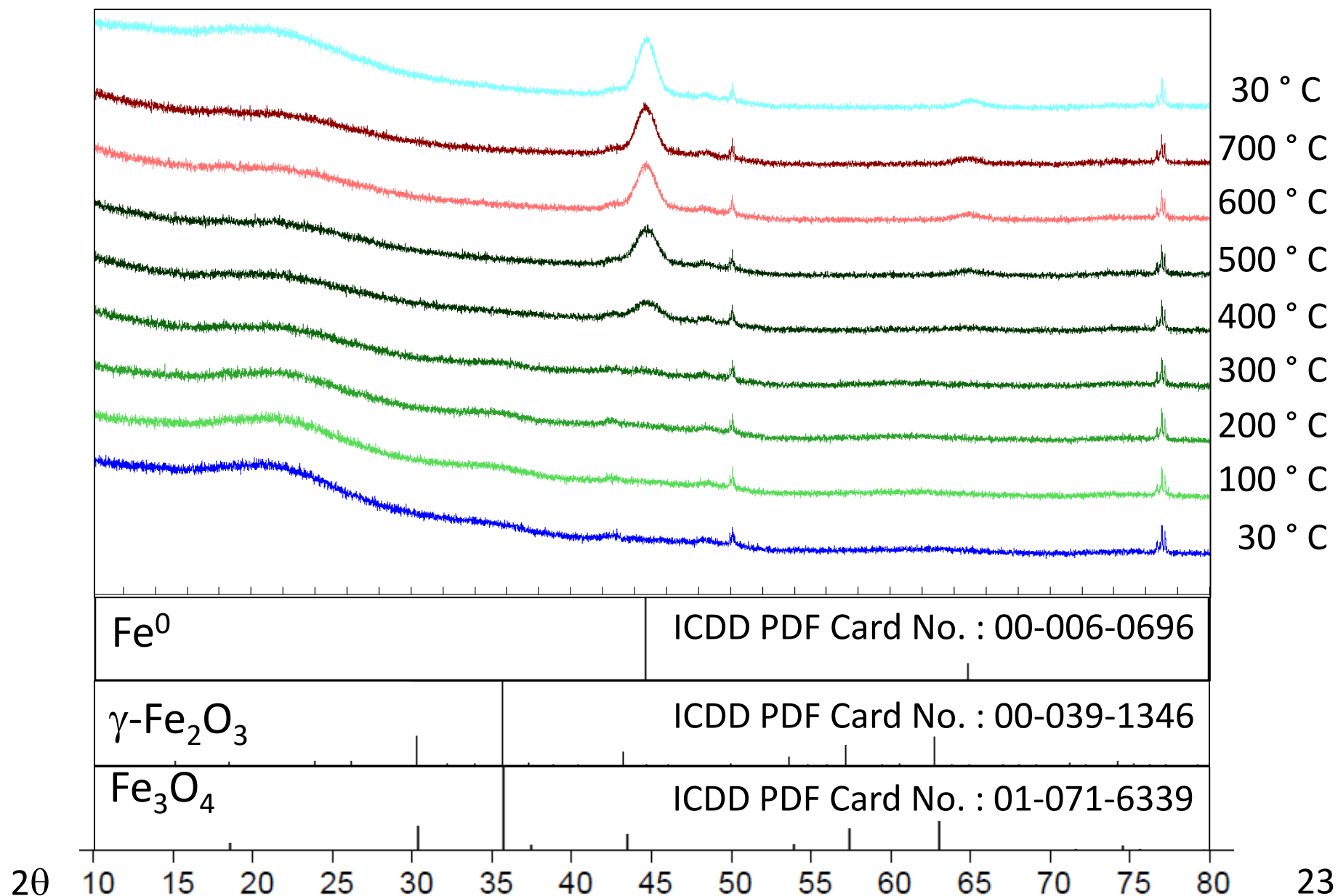




# Synthesis and Characterization

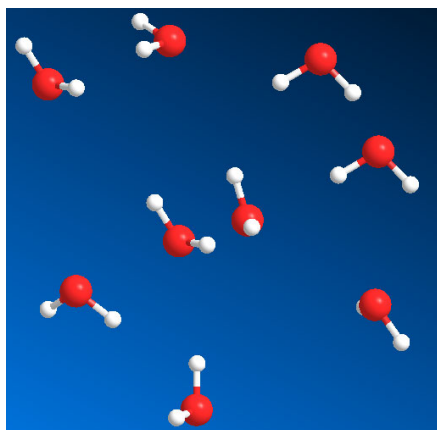
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# In-Situ XRD: 0.24%Pd/13.3%Fe<sub>2</sub>O<sub>3</sub>/A300



# Catalytic Activity

- This series of catalysts completely oxidizes under reaction conditions with H<sub>2</sub>O as solvent
- This series of catalysts undergoes majority oxidation under reaction conditions with hexadecane as solvent
- Liquid-phase kinetic data will need to wait for more stable catalysts

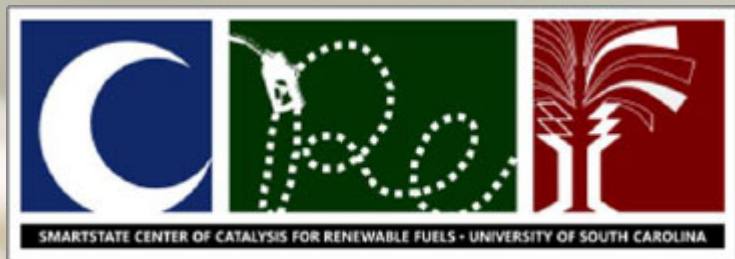


# Conclusions

- Pd-Fe prepared with SEA shows enhanced interaction in TPR
- The current array of catalysts oxidizes under reaction conditions
- Future work requires further catalyst design and synthesis for enhanced stability during liquid-phase HDO

# Acknowledgements

- National Science Foundation IGERT Grant
- Smartstate Center of Catalysis for Renewable Fuels – University of South Carolina
- JR Group
- Dr. Monnier Group
- Dr. Lauterbach Group





# Questions?

# References

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2. Huber, G. W.; Iborra, S.; Corma, A., Synthesis of transportation fuels from biomass: chemistry, catalysts, and engineering. *Chemical Reviews* **2006**, *106* (9), 4044-4098.
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12. Hensley, A. J.; Hong, Y.; Zhang, R.; Zhang, H.; Sun, J.; Wang, Y.; McEwen, J.-S., Enhanced Fe<sub>2</sub>O<sub>3</sub> reducibility via surface modification with Pd: Characterizing the synergy within Pd/Fe catalysts for hydrodeoxygenation reactions. *ACS Catalysis* **2014**, 4 (10), 3381-3392.