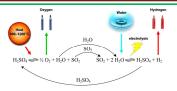
# Boron nitride: An effective support to synthesize very stable Pt-Ir catalyst for high temperature H<sub>2</sub>SO<sub>4</sub> decomposition

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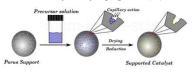
## Background



- □ H<sub>2</sub>SO<sub>4</sub> decomposition occurs catalytically at ≥800°C.
- ☐ As literature showed TiO<sub>2</sub> supported Pt-nanoparticles are effectively catalyze this decomposition reaction.
- ☐ However, at high temperature, platinum sinters and forms larger particles on TiO2 that deactivates the catalyst.
- ☐ The sintering of Pt can be reduced by stabilizing support or replacing support with more stable one
- ☐ Boron nitride (BN) exhibits higher thermal stability and oxidation resistance along with greater mechanical strength that could minimize Pt sintering at extreme conditions.

### **Experimental Methods**

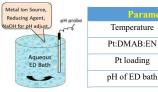
#### Monometallic Catalyst : Dry impregnation (DI)



- ☐ Drying: Overnight atmospheric drying and then dried @80°C for 6h in maffle furnace.
- ☐ Reduction: @300°C for 2h in hydrogen flow (Fresh)
- ☐ Calcination: @800°C for 8h in static air (Calcined)

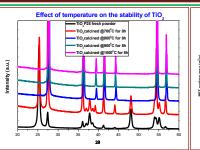
#### Bimetallic Catalyst : Electroless deposition (ED)

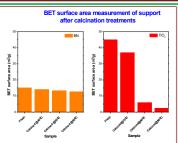
DMAB, (RA) M: Ir, Ru, Rh, Co, Fe etc.	Metal	Surface free energy (ergs/cm²)	
M M M	Cu	1934	
RA = Reducing Agent  Pt* Pt* Pt*  M M M M M	Pd	2043	
	Ni	2364	
	Pt	2691	
	Co	2709	
	Rh	2828	
	Mo	2877	
	Fe	2939	
Pt Pt Pt M M	Nb	2983	
	Re	3109	
Pt deposits Catalytically (on Ir) or Autocatalytically (on Pt)	Ir	3231	
	Ru	3409	

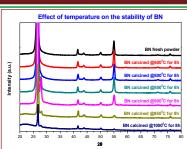


- ☐ Preparation: Deposition of metals by a pre-existing metal (catalysis) or the metal which is being deposited (auto
- ☐ Washing: Washed with DI-water to remove residual base
- ☐ Drying: Vacuum drying for 8-10 hrs (Fresh)
- □ Calcination: @800°C for 8h in static air (Calcined)

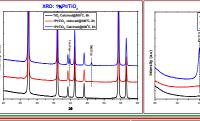
# Stabilization of supports

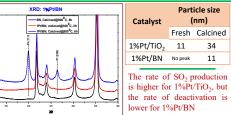


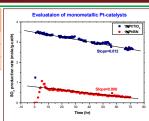


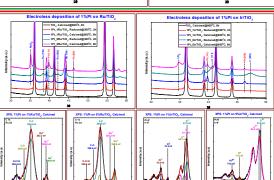


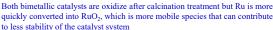
### Results and Discussions

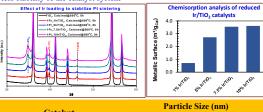




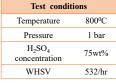








30	40 20	50	60	1,010	5"	1800	10,11
Catalyst	Particle Size (nm)						
	F	t	$IrO_2$				
1%Pt on 5	5%Ir/TiO <sub>2</sub> , Calc	ined	23	3.4		10.	0
1%Pt on 5	5%Ir/BN, Calcii	ned	12	2.3		16	5
1%Pt on 7	7.5%Ir/TiO <sub>2</sub> , Ca	lcined	21	1.6		8.5	0
1%Pt on 7	7.5%Ir/BN, Cal	eined	10	).5		10.	2



- □ 1%Pt/TiO<sub>2</sub> is the most active catalyst to produce SO2, but the rate of deactivation is the highest.
  - ☐ The activity of 1%Pt on 7.5%Ir/BN is consistent in 72 hrs of testing, the rate of catalyst deactivation is <0.015%/hour
  - ☐ The activity of catalysts are decreased with increasing loading of iridium.

#### Conclusion

- ☐ Almost 87% of the surface area has been lost for TiO₂ due to the calcination treatment at 800°C while BN is relatively stable.
- lacksquare The surface area obtained after calcination of BN is as double as the surface area obtained for TiO2.
- ☐ Ru is rapidly oxidize compare to Ir in high temperature oxidative condition and RuO2 is more mobile specie that may reduce of catalyst activity.
- ☐ TiO<sub>2</sub> supported monometallic Pt-catalyst is the most active catalyst compare to any other catalysts prepared on both BN and TiO2 support. However, the rate of deactivation is also high.
- ☐ The activity of the BN supported Pt-Ir catalysts is half of the activity of 1%Pt/TiO2, but the activity is very stable over 72 hours of testing.

#### Acknowledgement



50°C

1:5:4

1%

~10









# References

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